

- •Phase transitions
- Phase boundaries
- Phase transition temperature
- Melting point
- •Boiling point
- •Triple point
- Critical point
- Polymorphic forms
- Thermodynamics vs kineticsMetastable phases













#### 273.16 K





















*T*=373.15 K and *P*=1 bar



Vapour and liquid are in mutual equilibrium only for (P,T) values on the line



Intermezzo: in open system



@ T<sub>vap</sub> = 373.15 K Water starts to boil as

 $P_{\rm H_2O}(\rm air) < 1 bar$ 





The chemical potential of phase i (i = l, g) (Study guide p.11-13)

Note: we are dealing with a unary system

$$\mu_i \equiv G_{i,m}$$
 (pure compound) <sup>19</sup>

## Importance of the chemical potential:

Equilibrium between phases

$$H_2O(l) \leftrightarrow H_2O(g)$$























28





## Phase transitions in phase diagrams of unary systems





#### Phase transitions in phase diagrams of unary systems





### Phase transitions in phase diagrams of upary systems



#### Phase transitions in phase diagrams of unary systems



#### Ehrenfest classification of phase transitions



## Polymorphic (solid state) phase transitions



### Polymorphic solid state phase transitions



## Polymorphic solid state phase transitions



Characterized using Differential Scanning Calorimetry

#### Kinetic roughening transition for naphthalene crystals in a toluene solution



#### $a \rightarrow d$ : increasing driving force for crystallization





What about mixtures of compounds in the phases? 42

## Importance of the chemical potential:

Equilibrium between phases

$$H_2O(\alpha) \leftrightarrow H_2O(\beta)$$

in equilibrium:

 $\mu_{\alpha} = \mu_{\beta}$ 







#### binary phase diagram

in equilibrium: 
$$\mu_{i,\alpha} = \mu_{i,\beta} \begin{bmatrix} \frac{\text{phases } \alpha, \beta, \gamma, \dots}{1, \alpha, \beta} \end{bmatrix}$$

Equilibrium between *P* phases of components *i* in mixtures

C components in each phase

P phases in mutual equilibrium



$$\frac{\text{\# independent variables}}{dG = VdP - SdT + \sum_{j=\alpha}^{P} \sum_{i=1}^{C} \mu_{i,j} dn_{i,j}} \xrightarrow{F \to P, T, x_1 \cdots x_C \to 2 + PC}$$

in equilibrium: 
$$\mu_{i,\alpha} = \mu_{i,\beta} \begin{bmatrix} \frac{\text{phases } \alpha, \beta, \gamma, \dots}{\text{components } i = 1, 2, 3, \dots} \end{bmatrix}$$

#### Equilibrium between P phases of components i in mixtures



47

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 $F \rightarrow 2 + P(C-1) - (P-1)C = C - P + 2$ 



in equilibrium: 
$$\mu_{i,\alpha} = \mu_{i,\beta} - \begin{bmatrix} \frac{\text{phases } \alpha, \beta}{\text{components } i} \end{bmatrix}$$

#### Equilibrium between P phases of C components in mixtures

<u>*C* components in the mixtures</u> <u>*P* phases in mutual equilibrium</u> F = C - P + 2



Temperature, T

#### unary phase diagram



#### **Gibbs phase rule**

$$F = C - P + 2$$

*F*: # degrees of freedom*C*: # components*P*: # phases



#### **Gibbs phase rule**

$$F = C - P + 2$$

Temperature, T

#### unary phase diagram



#### **Gibbs phase rule**

$$F = C - P + 2$$

Temperature, T

#### unary phase diagram



#### **Gibbs phase rule**

$$F = C - P + 2$$

Temperature, T

unary phase diagram