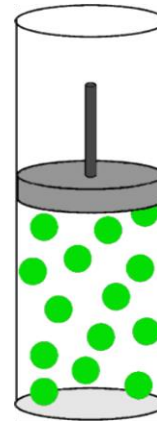
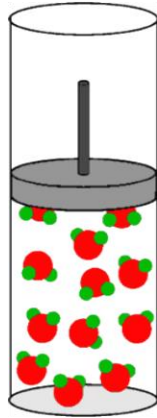
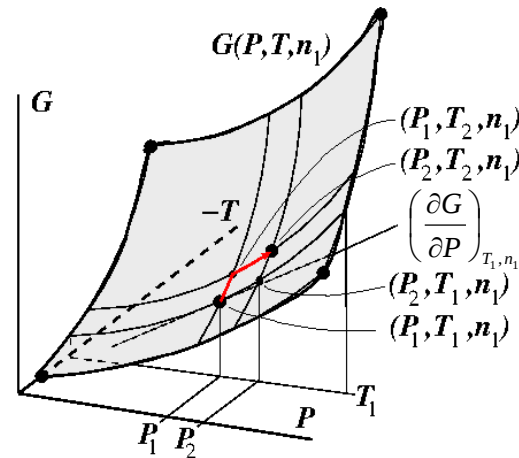
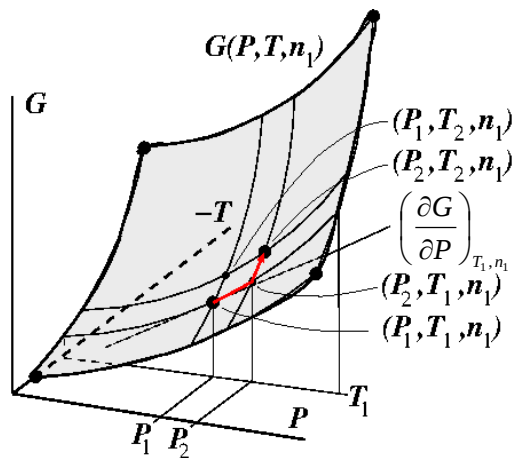


Summary of Lecture 1

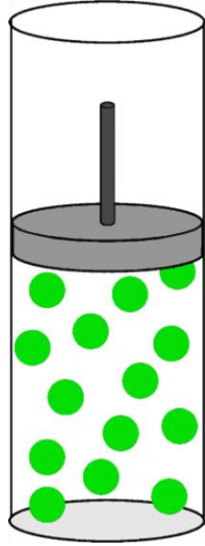
- Molecular (perfect) gases vs atomic gases



- Total differential of (thermodynamic) functions



Molecular (perfect) gases vs atomic gases



Perfect gas

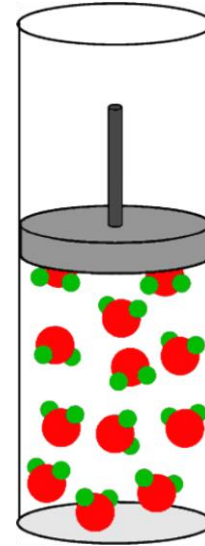
$$PV = nRT$$

obeys **equipartition theorem**

(high T and low P)

$$U = \frac{1}{2} kT$$

per degree of freedom



Atomic perfect gas

(SG p.17-18)

Molecular perfect gas

$$U = U^T = \frac{3}{2} NkT$$

$$Nk = nR$$

$$C_V = \frac{3}{2} nR$$

$$C_V \equiv \left(\frac{\partial U}{\partial T} \right)_V$$

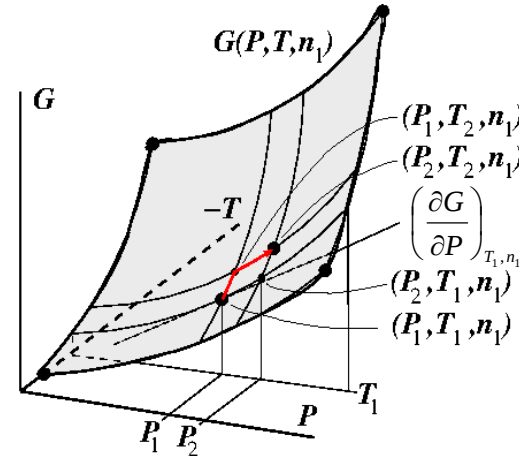
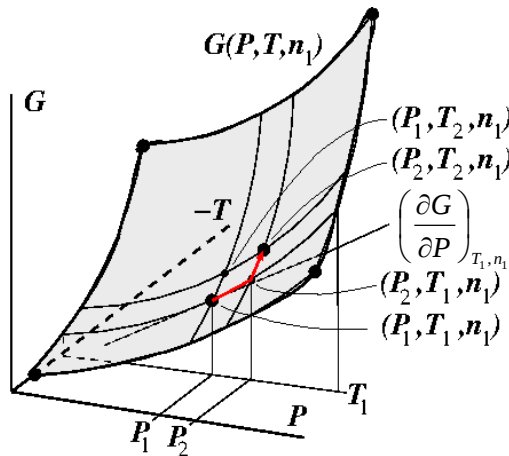
$$U = \left(3 + N_R + 2N_V \right) \frac{1}{2} MkT$$

$$Mk = nR$$

$$C_V = \left(3 + N_R + 2N_V \right) \frac{1}{2} nR$$

Total differential of (thermodynamic) functions

(Gibbs free energy G as an example)



$$\Delta G(P_1, T_1 \rightarrow P_2, T_2)|_n = \int_{P_1}^{P_2} \left(\frac{\partial G}{\partial P} \right)_{T_1, n} dP + \int_{T_1}^{T_2} \left(\frac{\partial G}{\partial T} \right)_{P_2, n} dT = \int_{T_1}^{T_2} \left(\frac{\partial G}{\partial T} \right)_{P_1, n} dT + \int_{P_1}^{P_2} \left(\frac{\partial G}{\partial P} \right)_{T_2, n} dP$$

Characteristic equ. G

$$dG = -SdT + VdP$$

G is state function

$$\left(\frac{\partial^2 G}{\partial T \partial P} \right) = \left(\frac{\partial^2 G}{\partial P \partial T} \right)$$

Maxwell relation

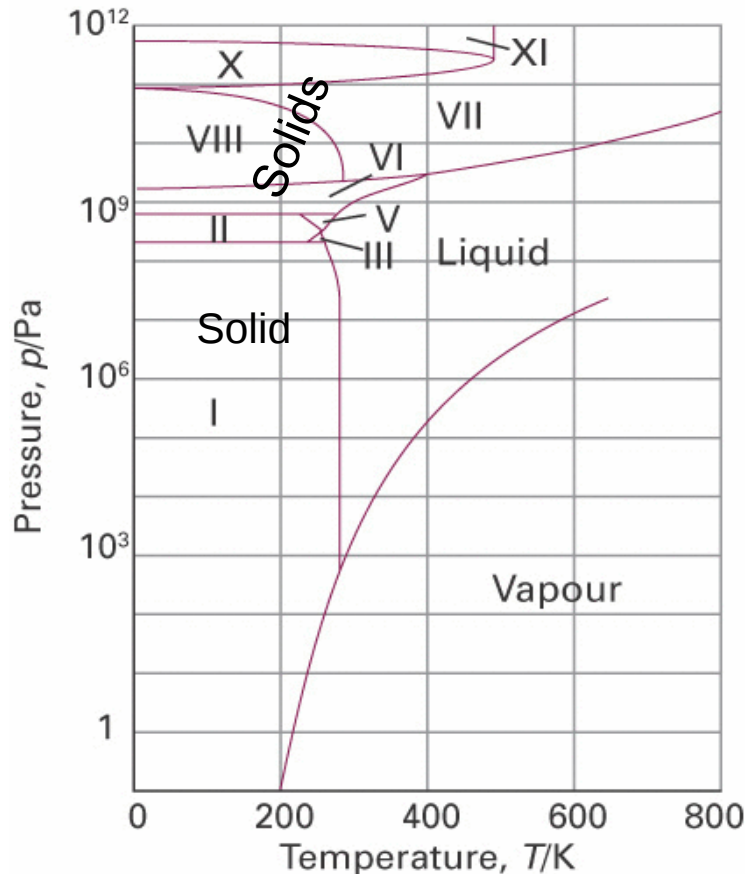
$$\left(\frac{\partial V}{\partial T} \right)_P = - \left(\frac{\partial S}{\partial P} \right)_T$$

Lecture 2

Phase diagrams and phase transitions of unary systems

Lecture 2

Phase diagrams and phase transitions of unary systems

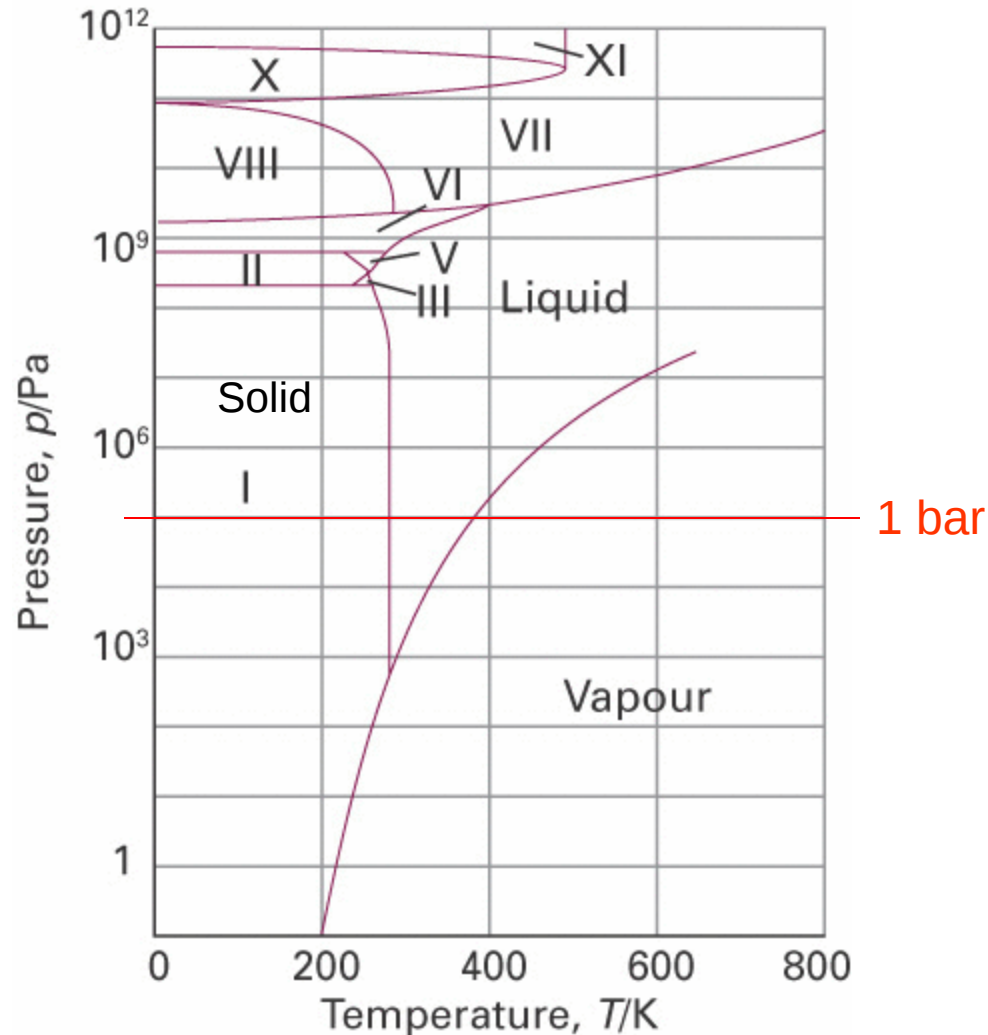


- Phase transitions
- Phase boundaries
- Phase transition temperature
- Melting point
- Boiling point
- Triple point
- Critical point
- Polymorphic forms

- Thermodynamics vs kinetics
- Metastable phases

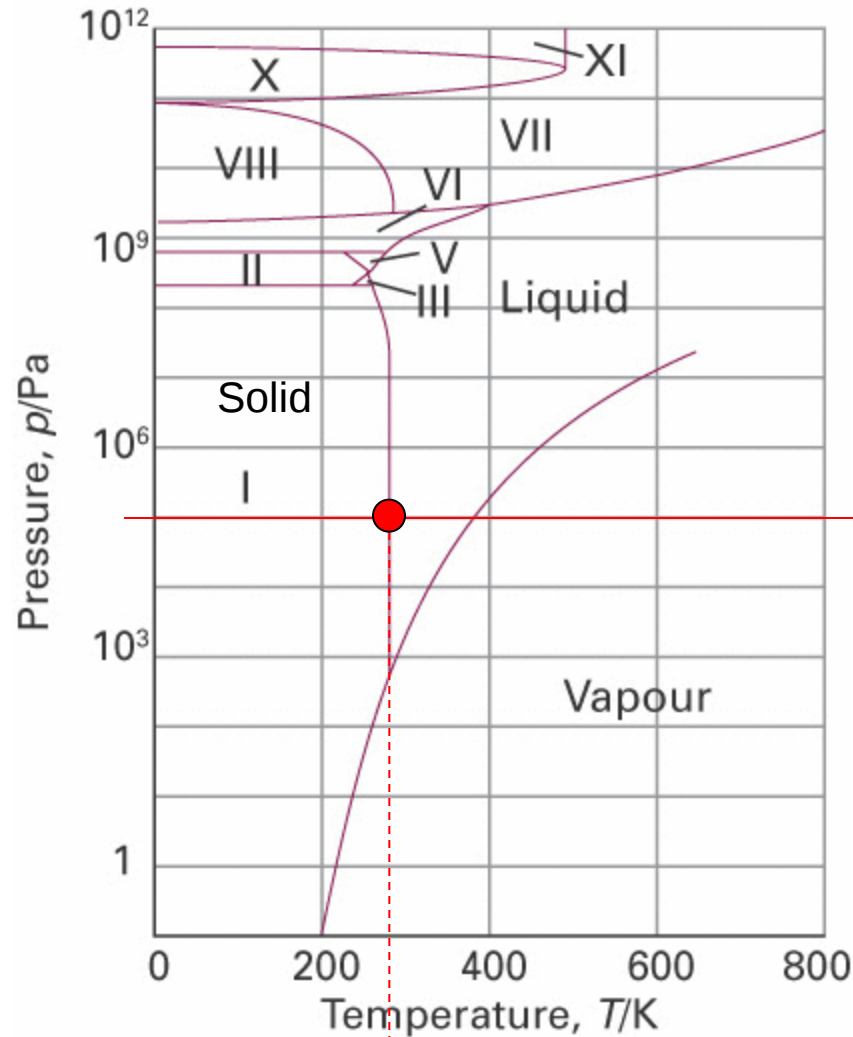
(Equilibrium) Phase Diagram H_2O

Phase diagrams and phase transitions of unary systems



(Equilibrium) P, T phase diagram H_2O

Phase diagrams and phase transitions of unary systems



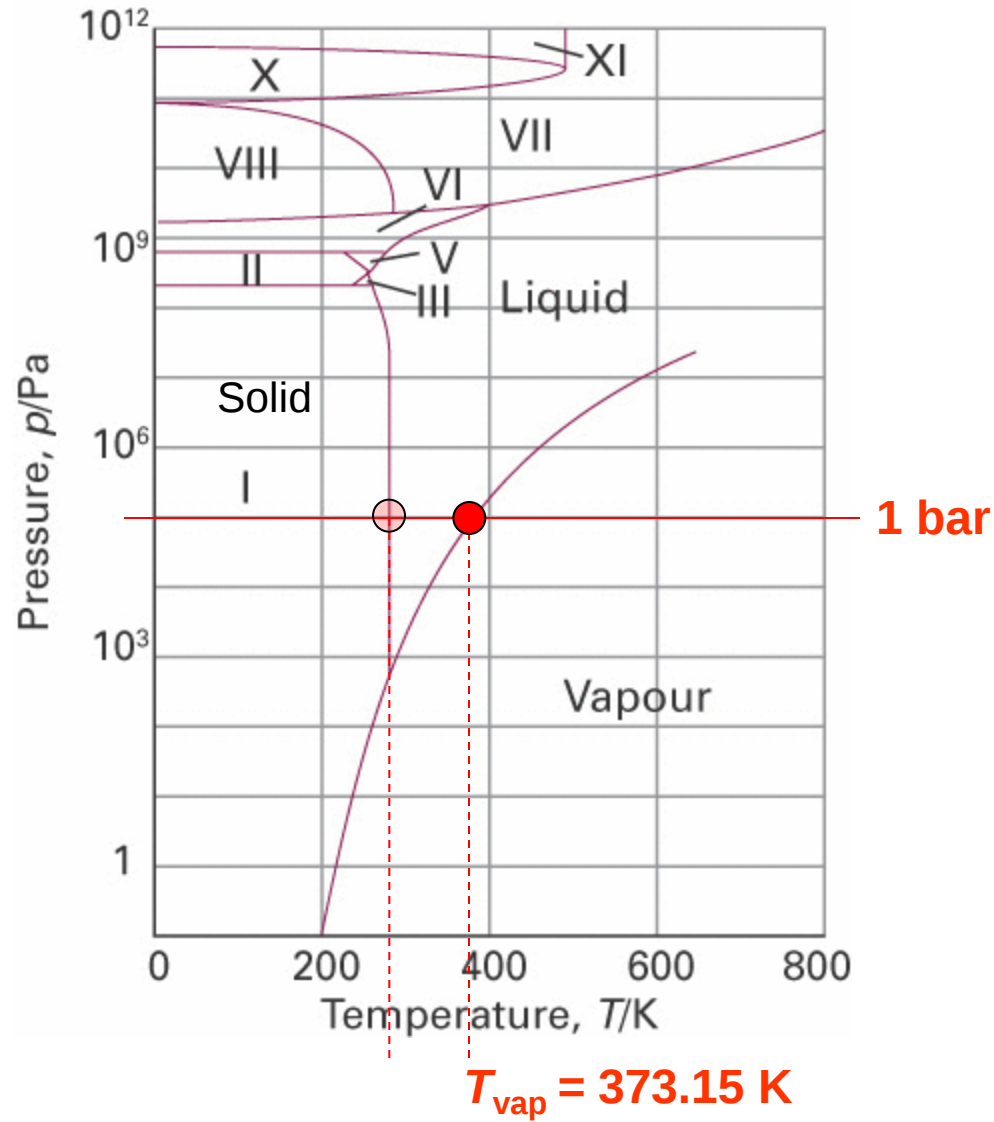
1 bar

$$T_{\text{fus}} = T_{\text{cryst}} = 273.15\text{ K}$$



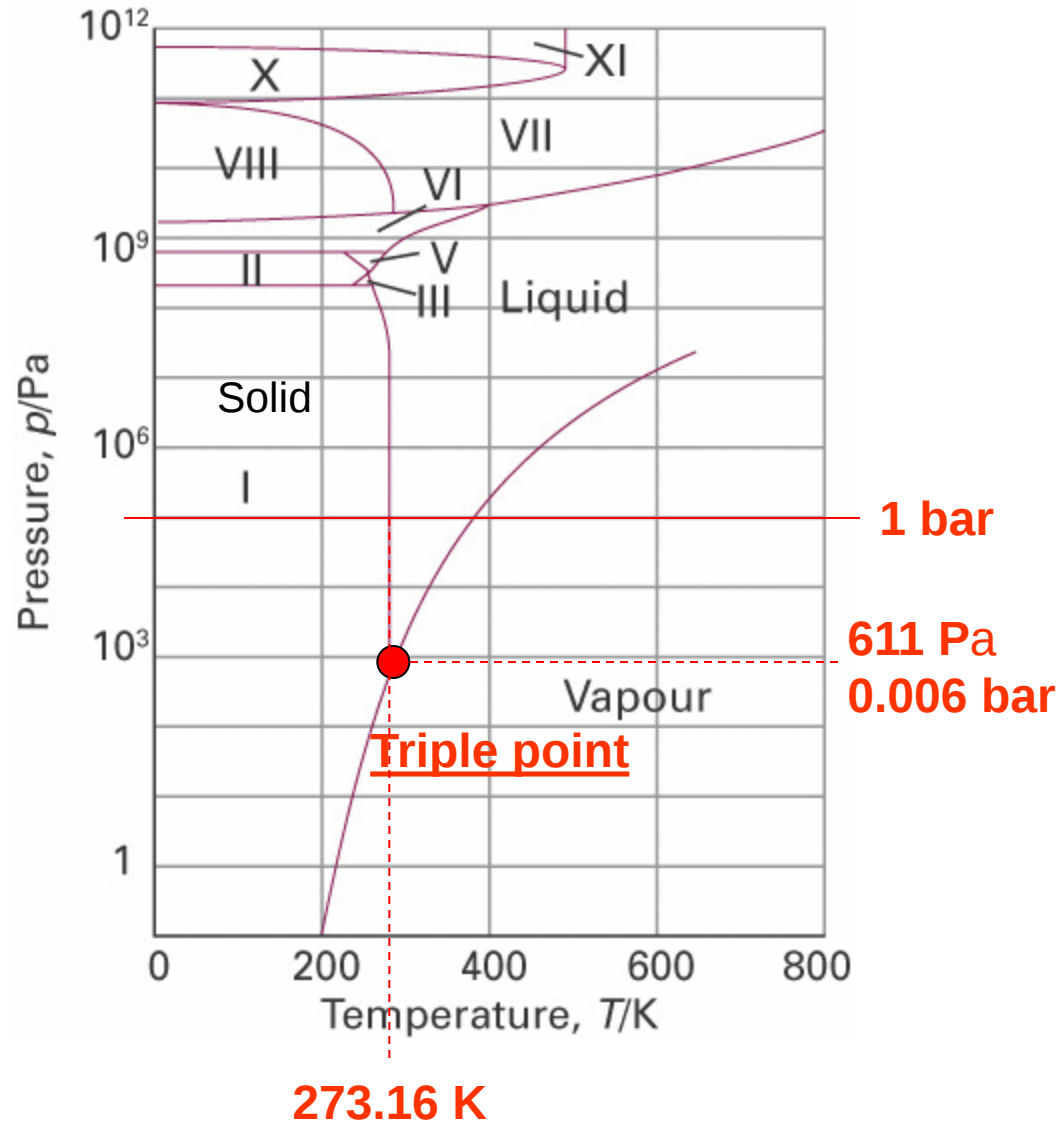
(Equilibrium) P, T phase diagram H_2O

Phase diagrams and phase transitions of unary systems



(Equilibrium) P, T phase diagram H_2O

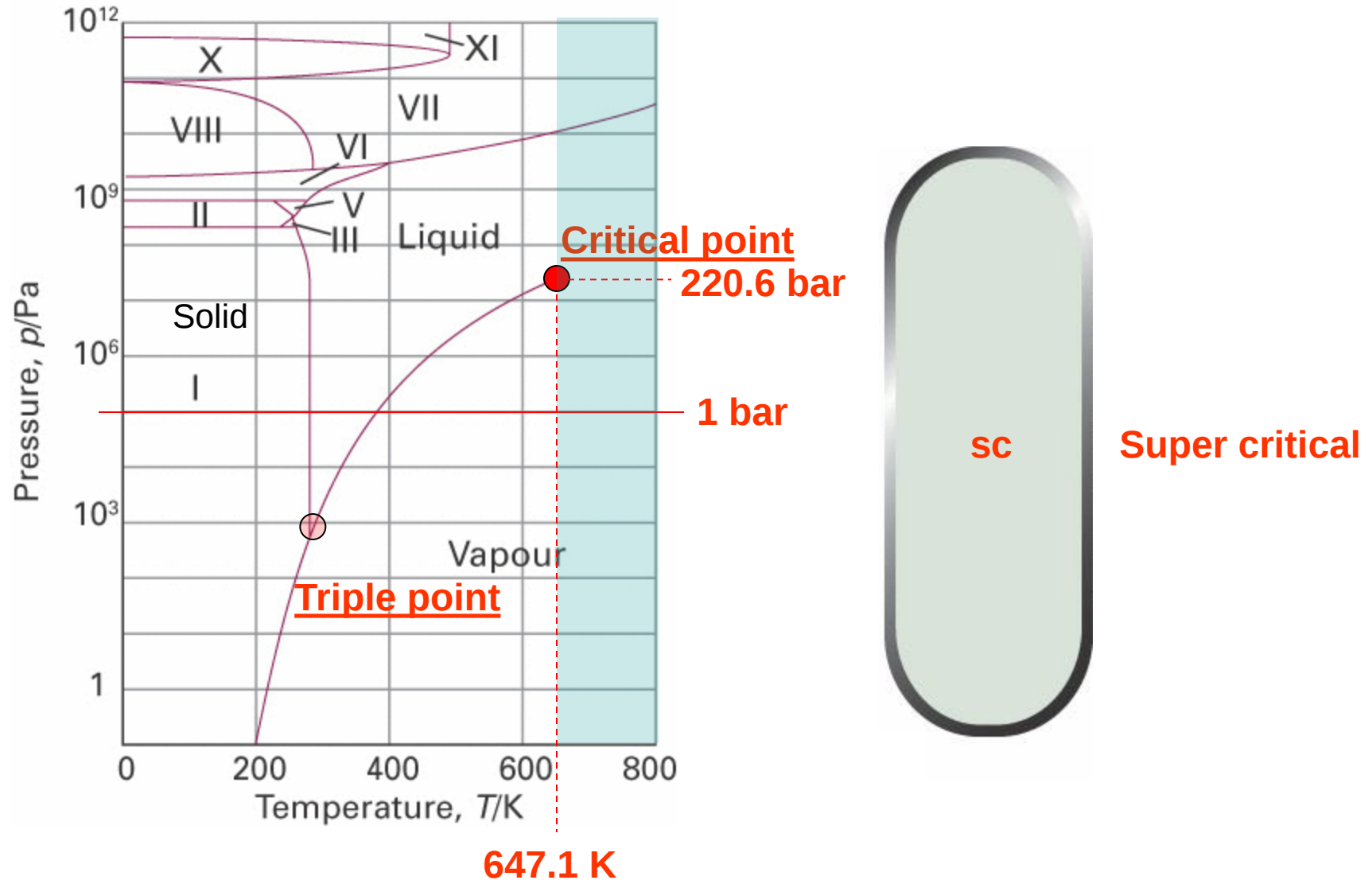
Phase diagrams and phase transitions of unary systems



[Youtube link](#)

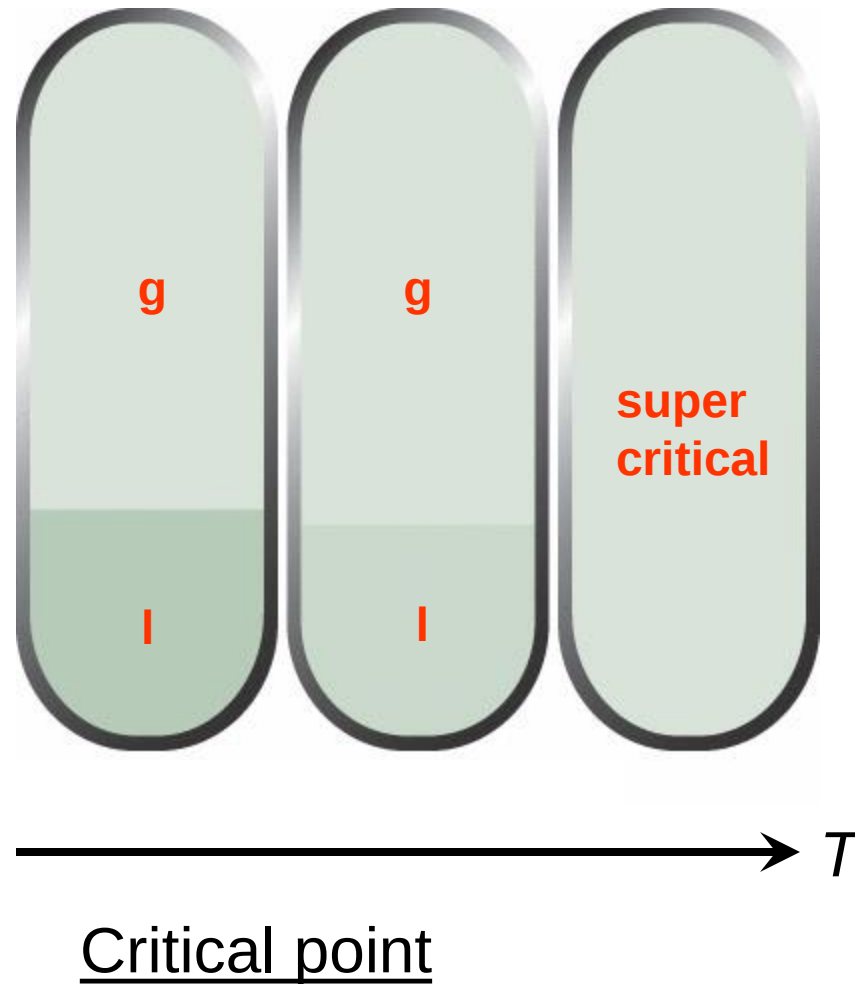
(Equilibrium) P, T phase diagram H_2O

Phase diagrams and phase transitions of unary systems

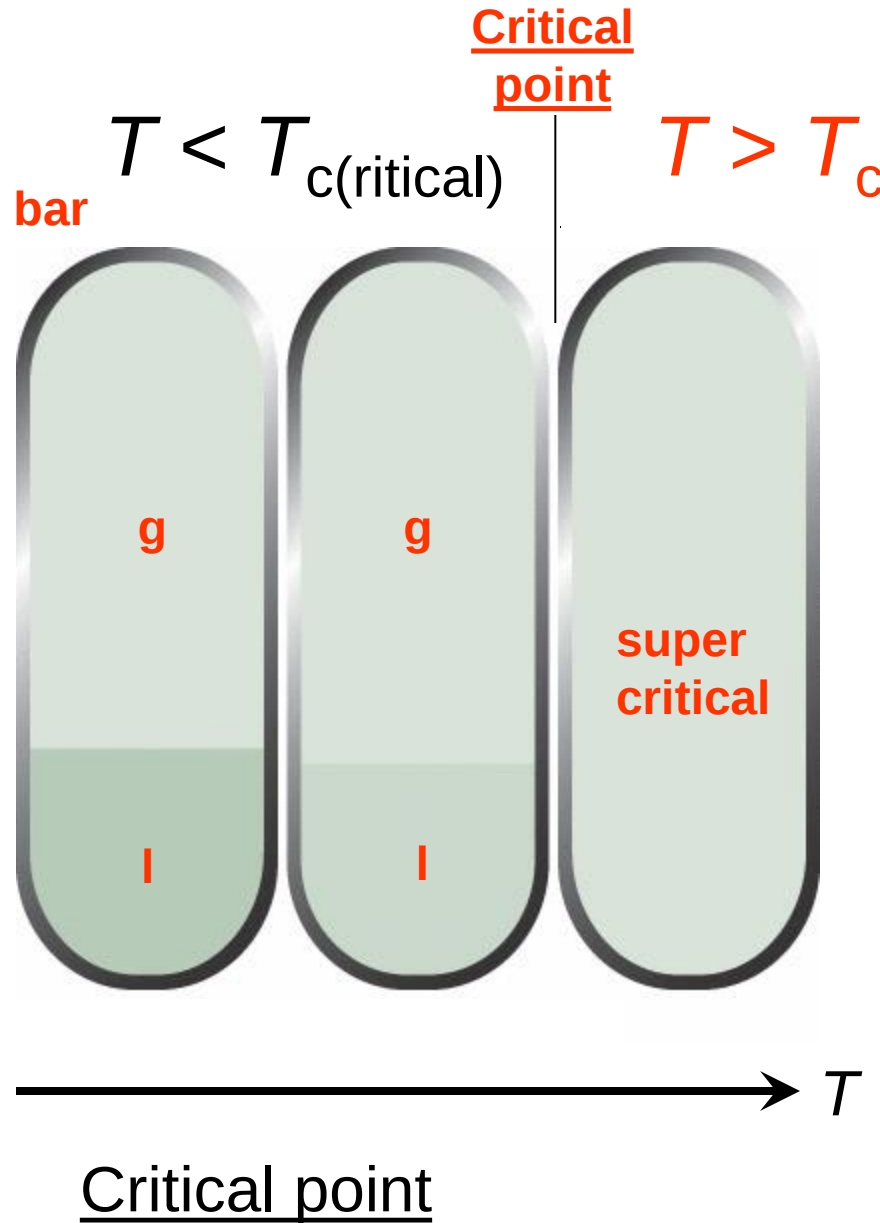
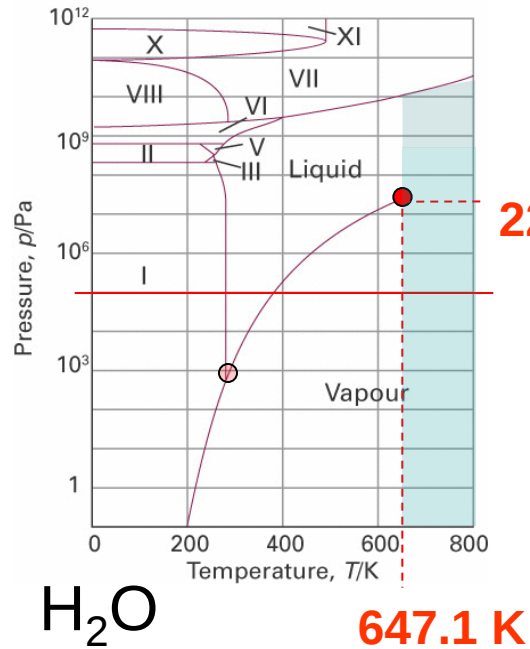


(Equilibrium) P,T phase diagram H_2O

Phase diagrams and phase transitions of unary systems

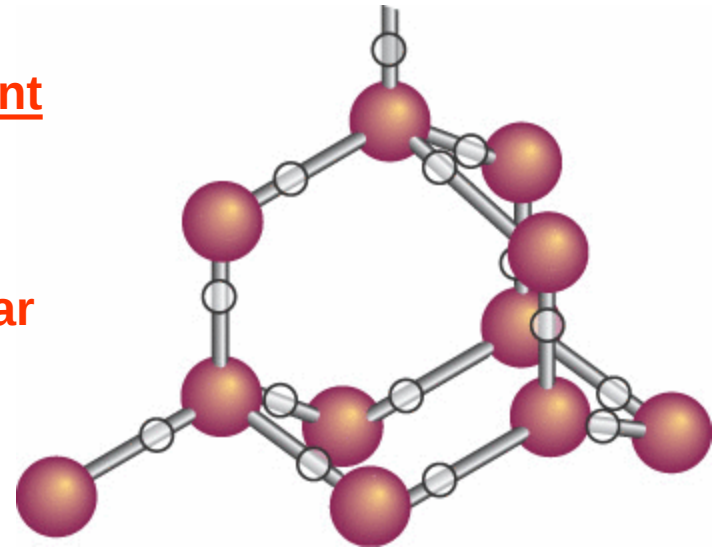
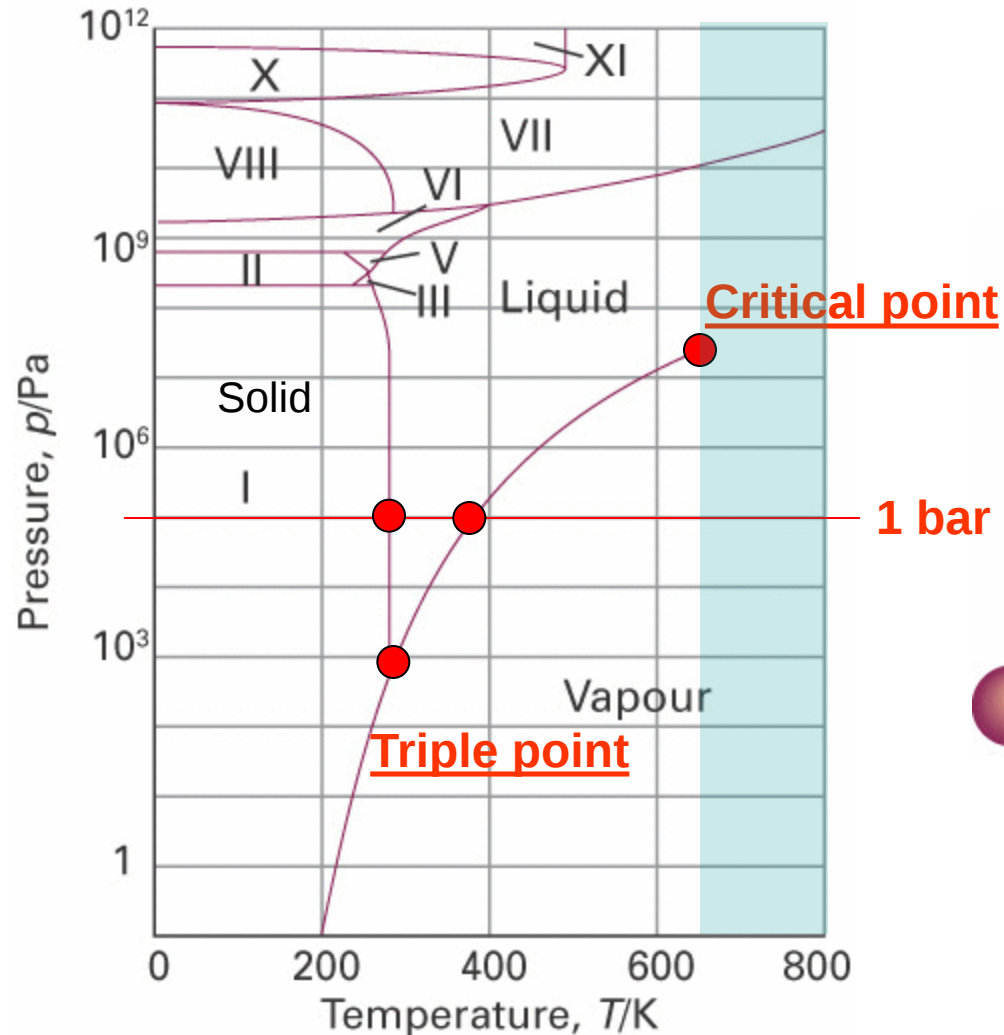


Phase diagrams and phase transitions of unary systems



[Youtube link](#)

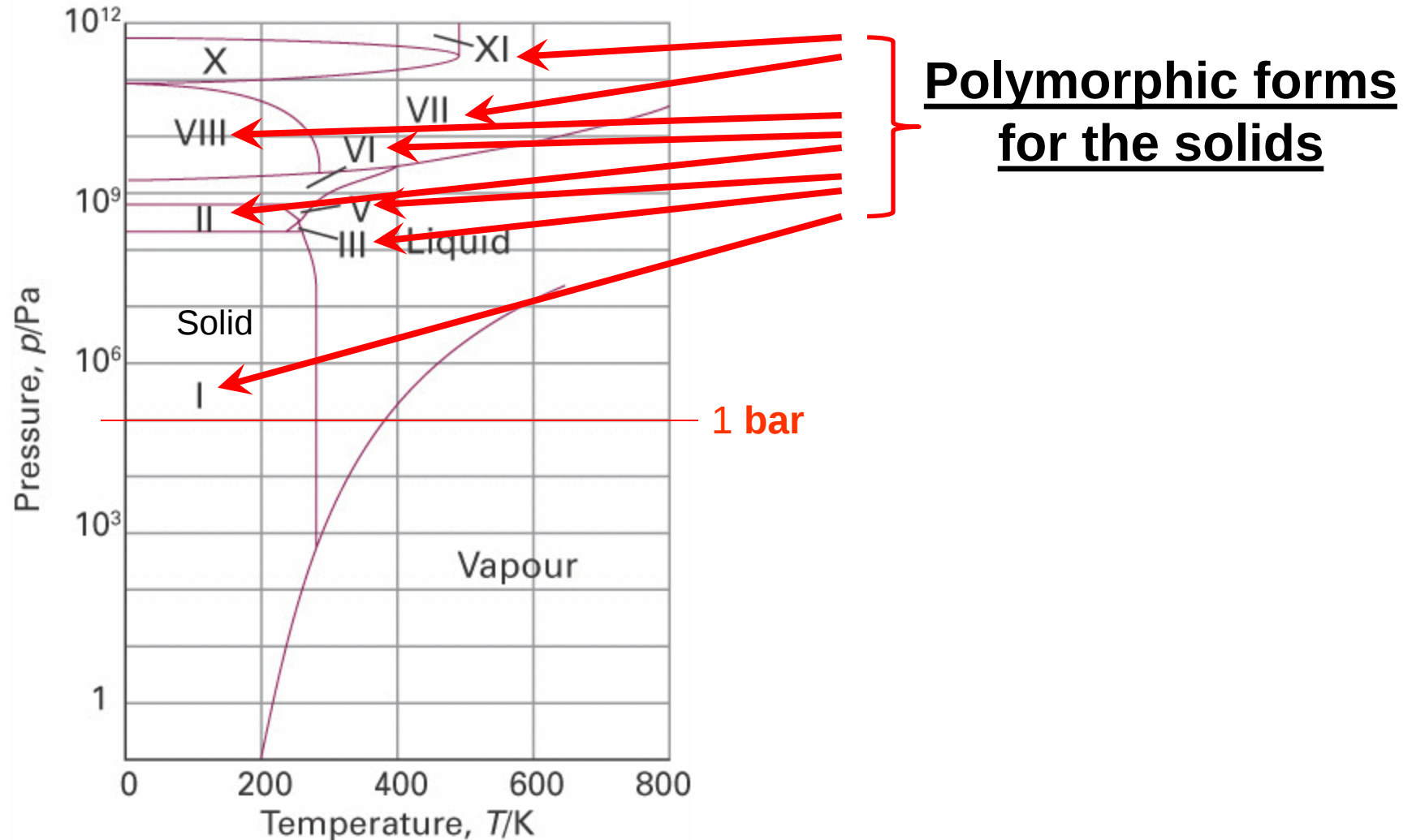
Phase diagrams and phase transitions of unary systems



H-bonding

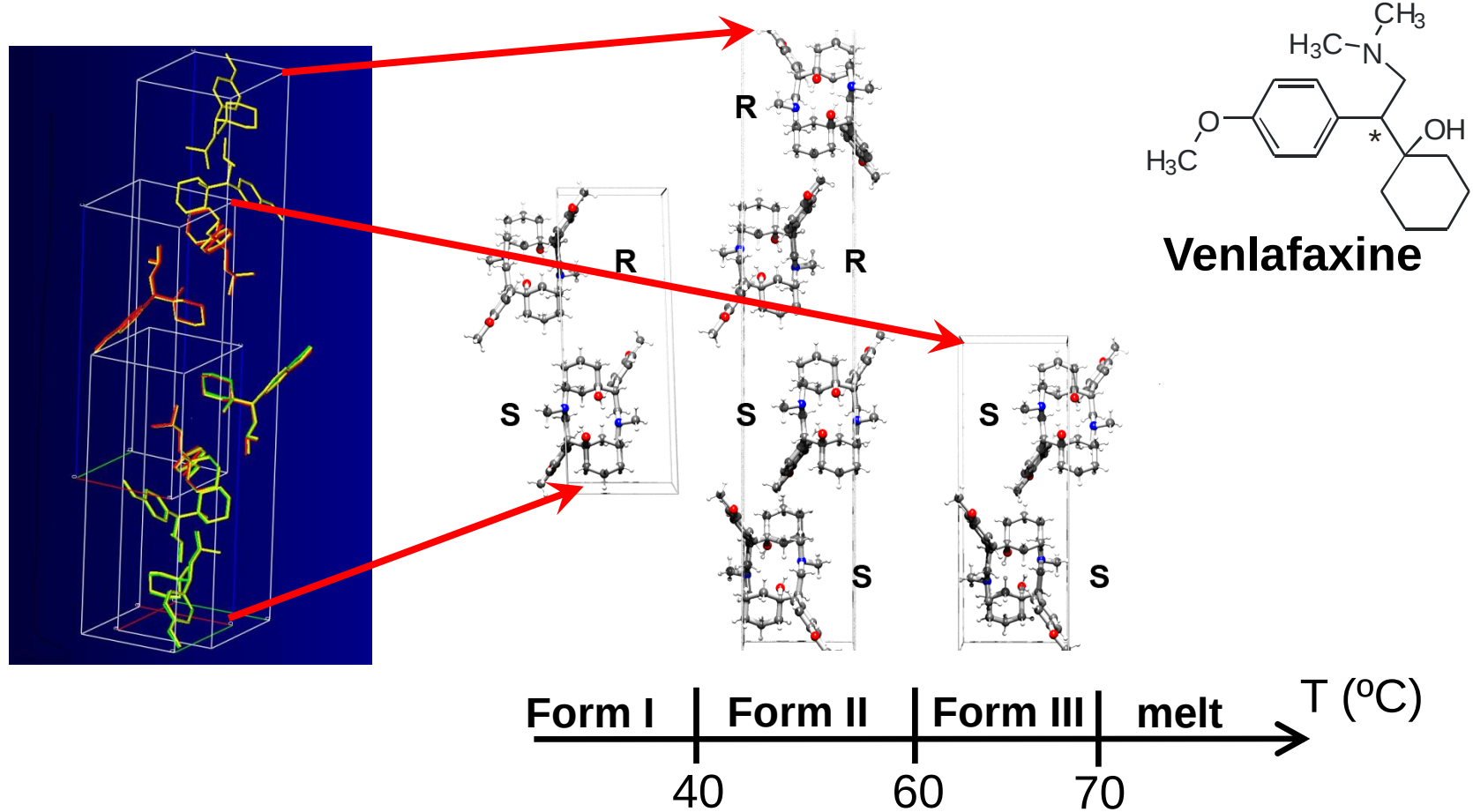
(Equilibrium) P, T phase diagram H_2O

Phase diagrams and phase transitions of unary systems



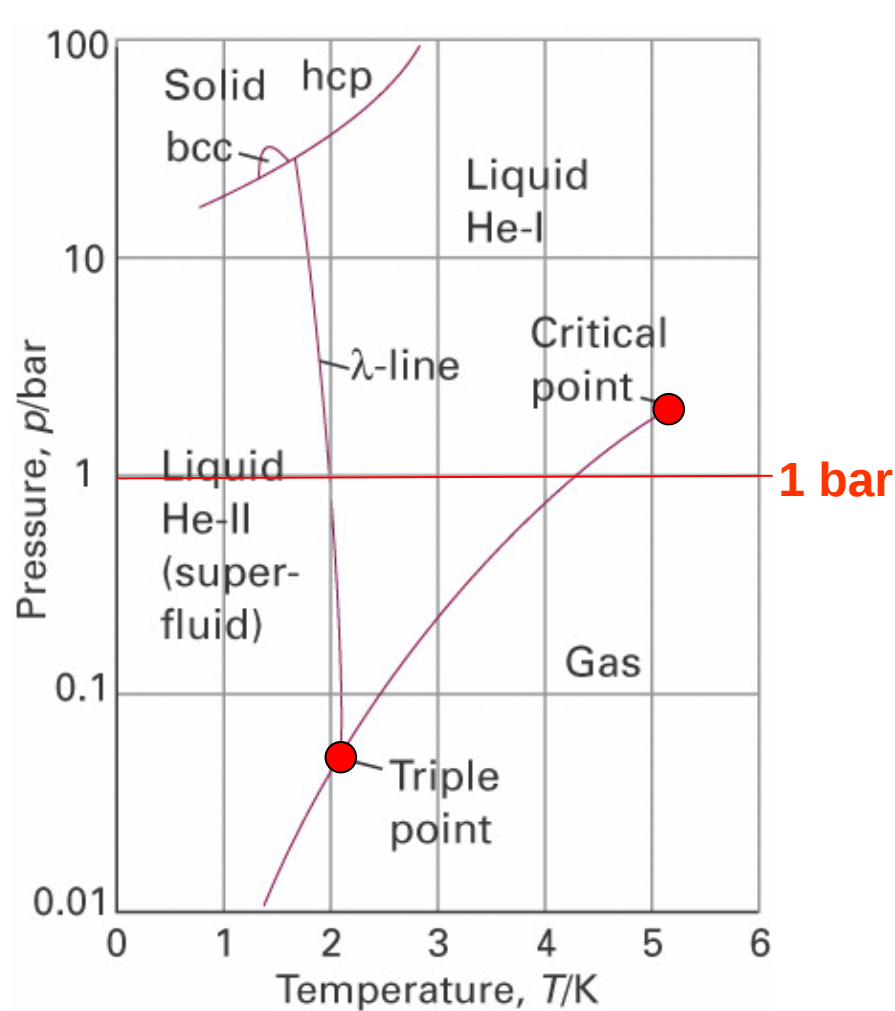
(Equilibrium) P, T phase diagram H_2O

Phase diagrams and phase transitions of unary systems

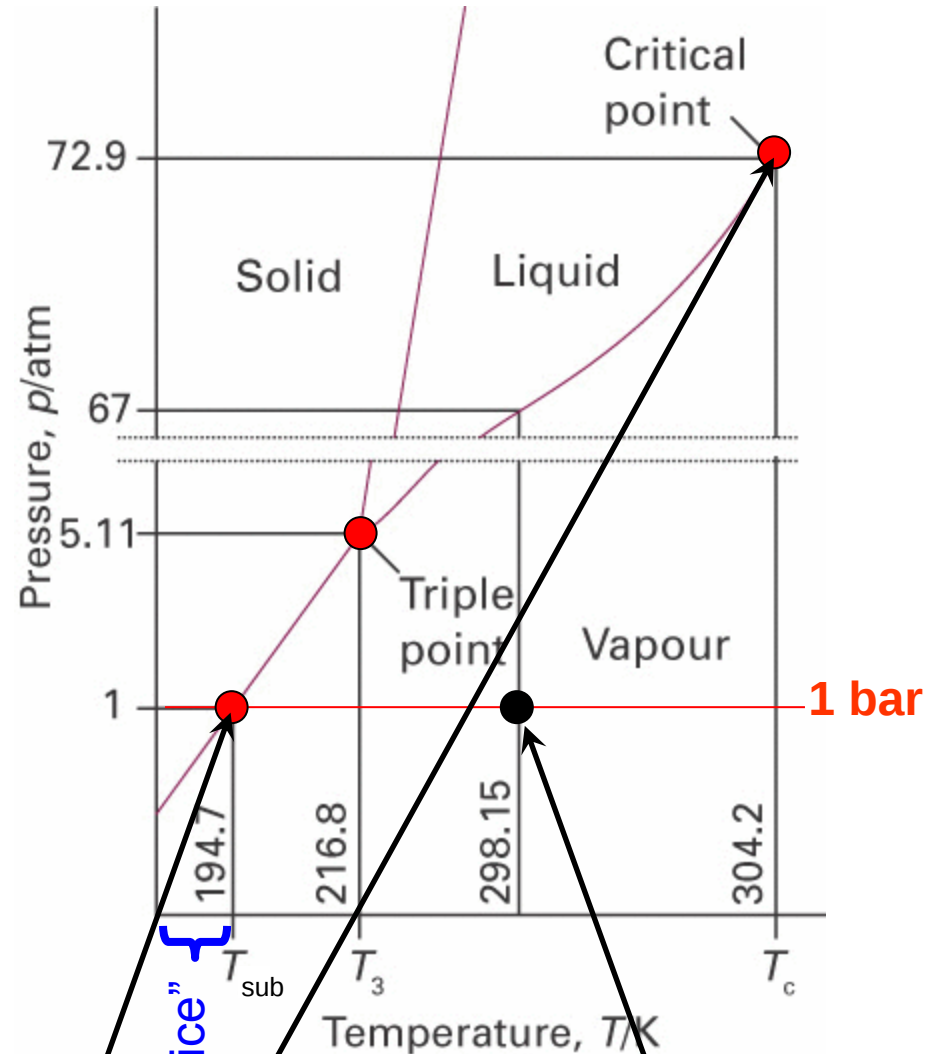


Polymorphic (solid state) phase transitions

Phase diagrams and phase transitions of unary systems



^4He



CO_2

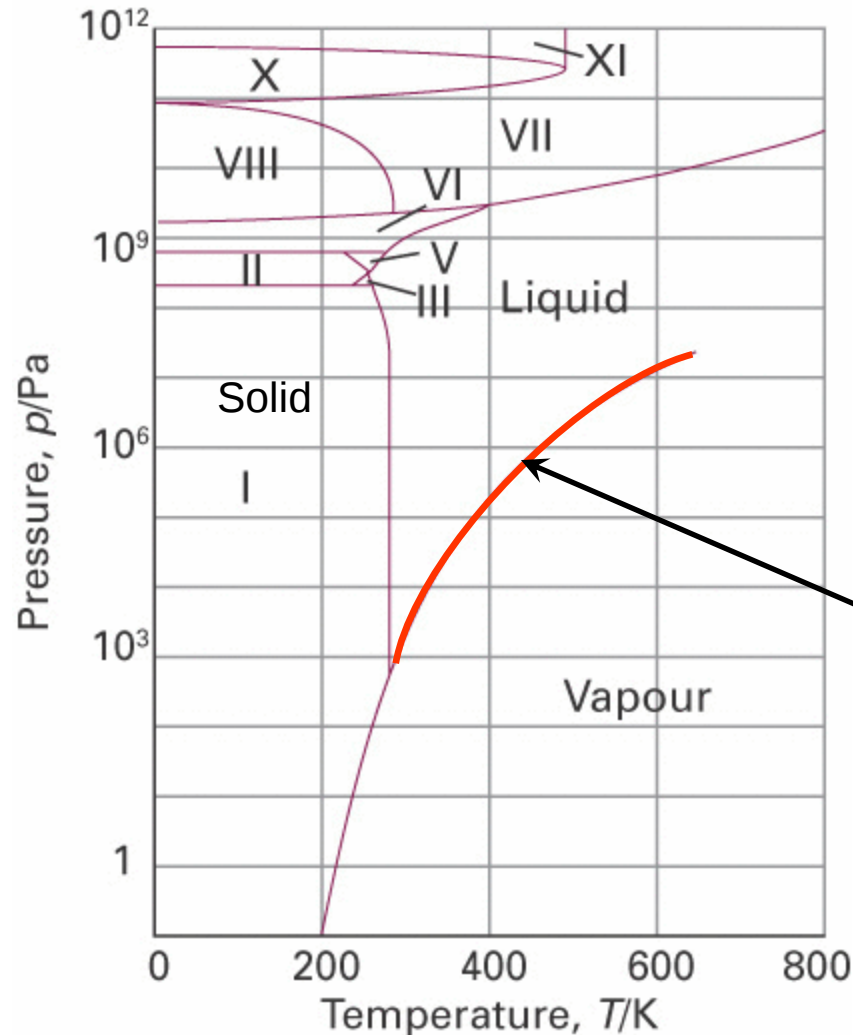
sublimation point at 1 bar

ambient conditions

See link on slide 12

Phase boundary lines in diagrams of unary systems

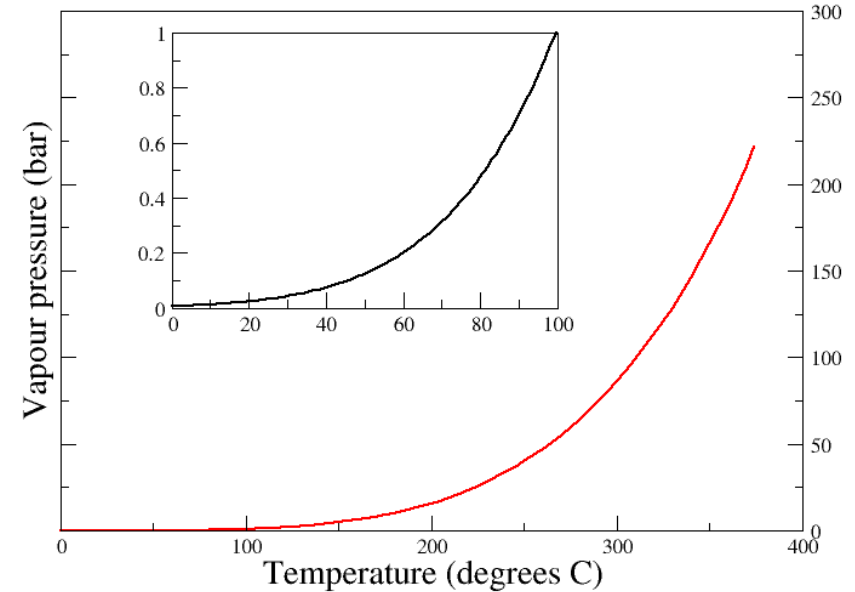
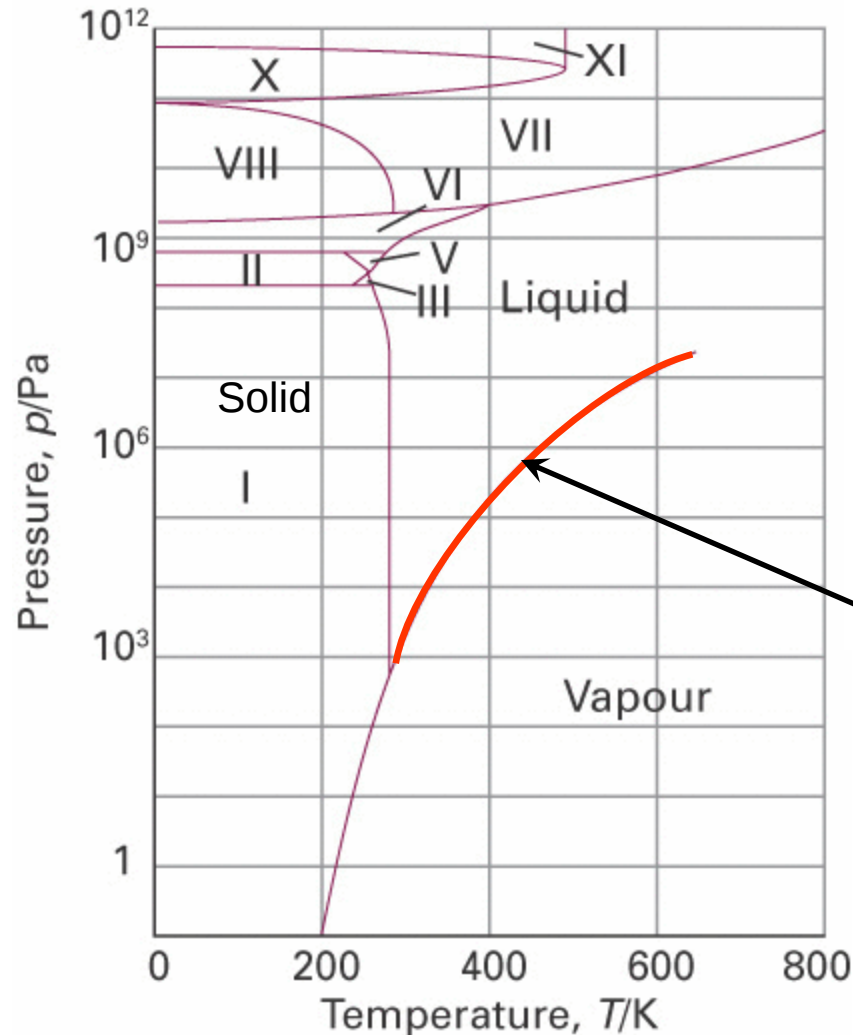
Phase boundary lines in diagrams of unary systems



Vapour and liquid are in mutual equilibrium only for (P, T) values on the line

(Equilibrium) P, T phase diagram H_2O

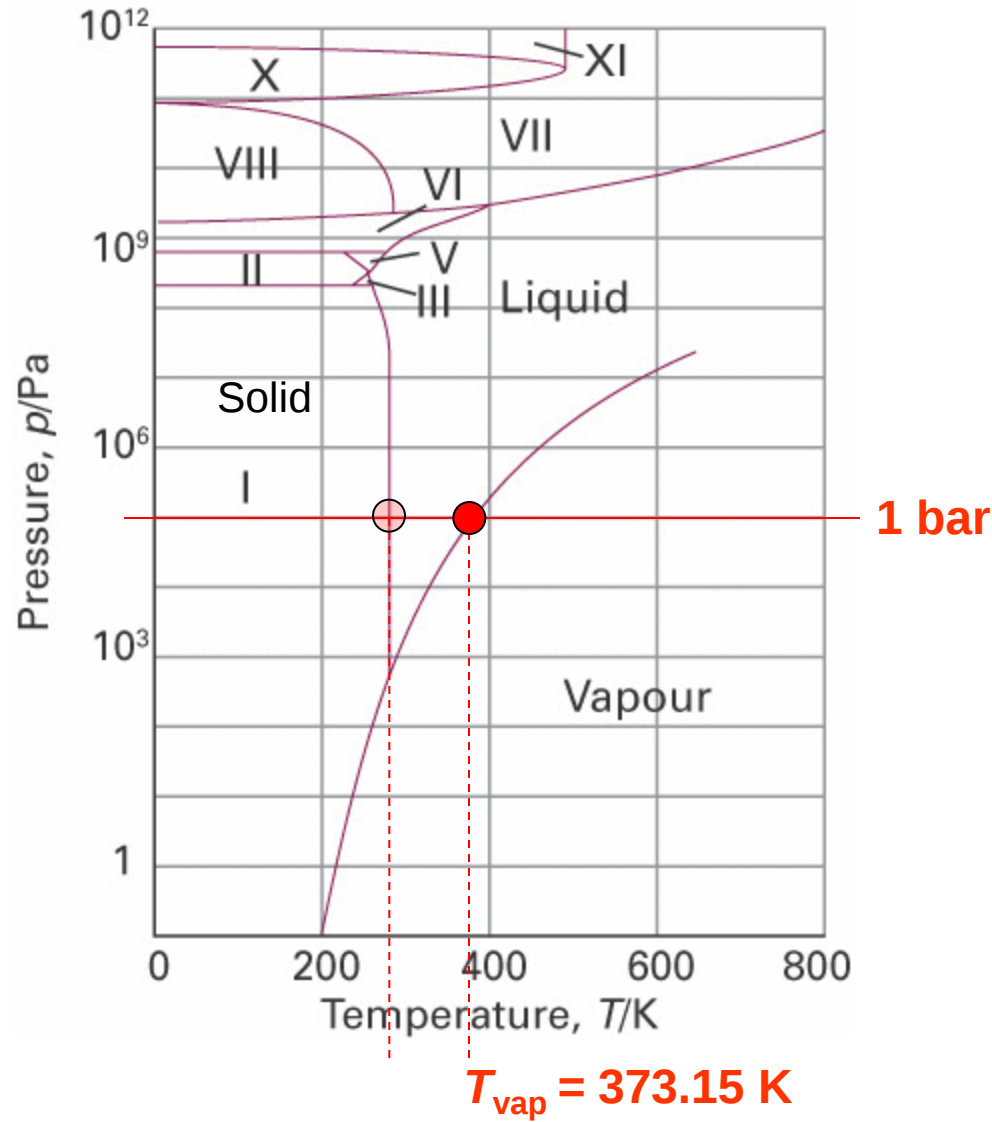
Phase boundary lines in diagrams of unary systems



Vapour and liquid are in mutual equilibrium only for (P, T) values on the line

(Equilibrium) P, T phase diagram H_2O

Phase boundary lines in diagrams of unary systems



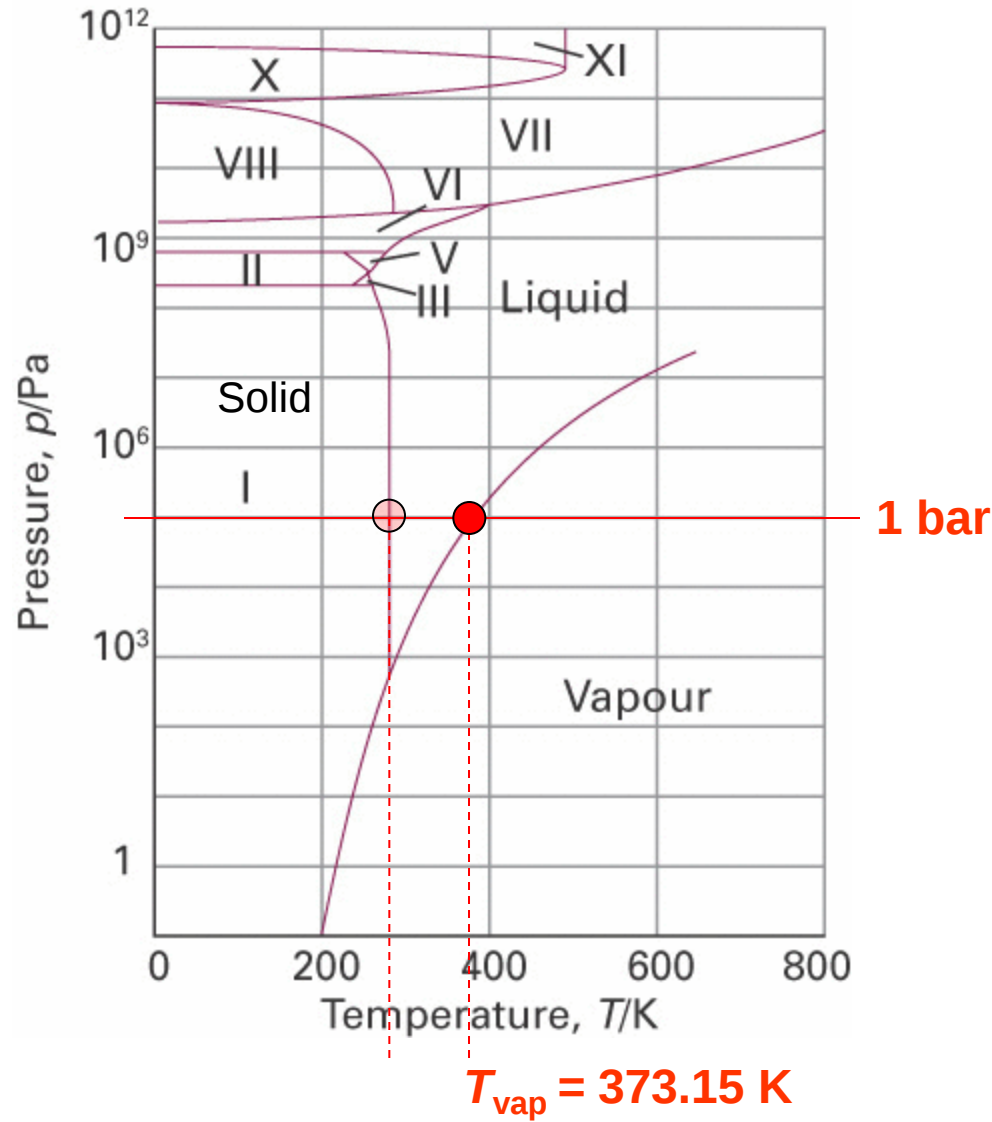
$T = 373.15 \text{ K}$ and $P = P^\theta = 1 \text{ bar}$



Vapour and liquid are in mutual equilibrium only for (P, T) values on the line

(Equilibrium) P, T phase diagram H_2O

Phase diagrams and phase transitions of unary systems



Intermezzo:
in open system



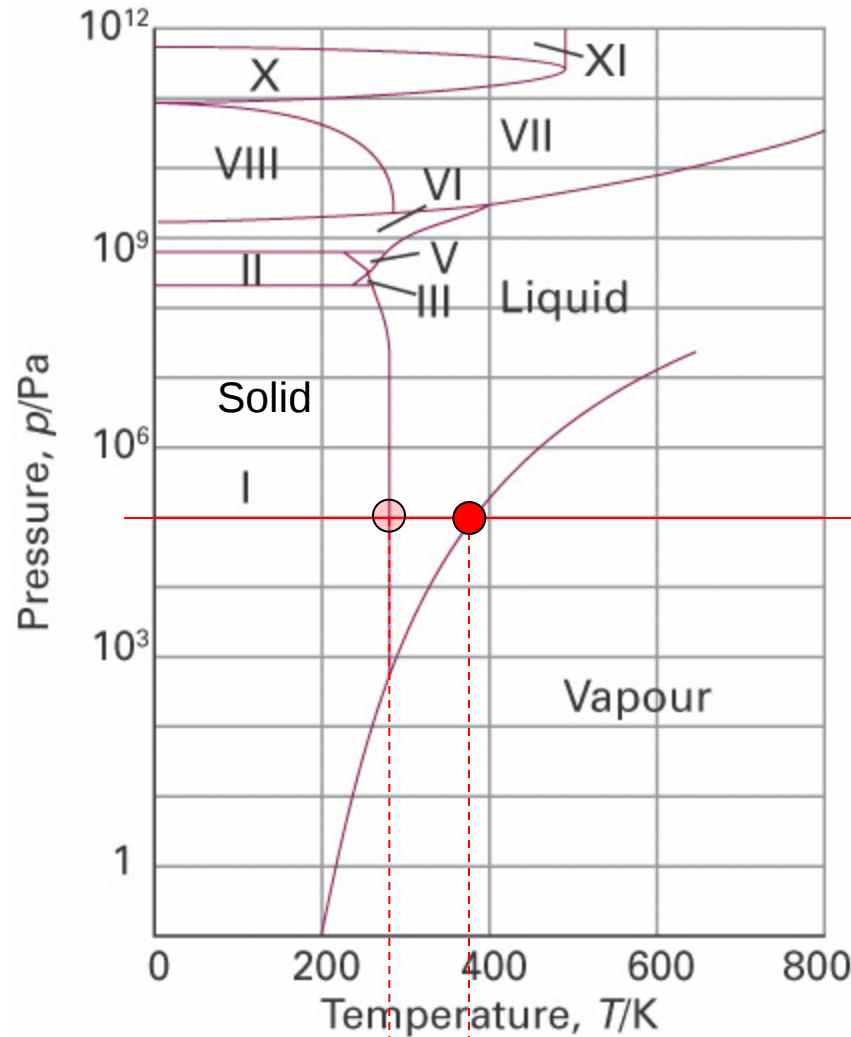
@ $T_{\text{vap}} = 373.15 \text{ K}$
Water starts to boil as

$$P_{\text{H}_2\text{O}}(\text{air}) < 1 \text{ bar}$$

Non-equilibrium
situation

(Equilibrium) P, T phase diagram H₂O

Phase diagrams and phase transitions of unary systems



$T_{\text{vap}} = 373.15 \text{ K}$

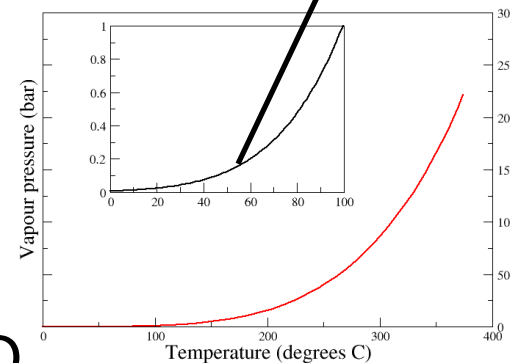
1 bar

Intermezzo:

Relative Humidity

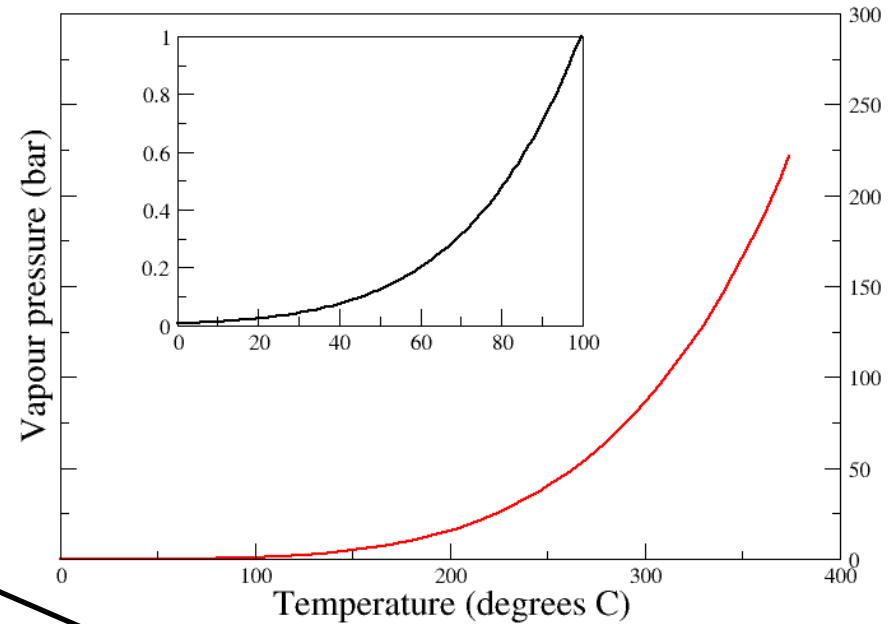
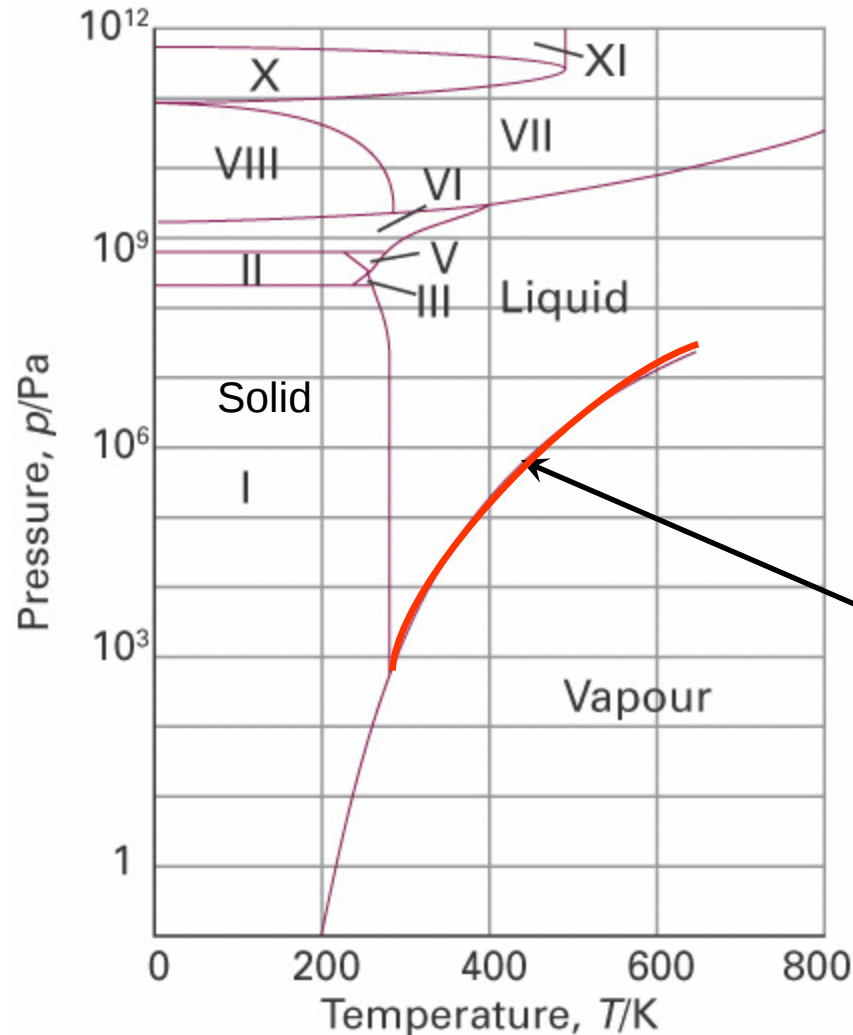
$$RH = \phi \equiv \frac{P_{\text{H}_2\text{O}}(\text{air})}{P_{\text{H}_2\text{O}}^*}$$

$RH < 100\% \rightarrow$
Non-equilibrium



(Equilibrium) P, T phase diagram H_2O

Phase boundary lines in diagrams of unary systems

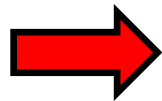
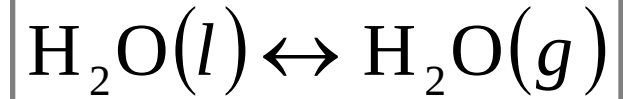


Vapour and liquid are in mutual equilibrium only for (P, T) values on the line

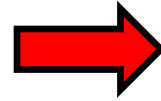
(Equilibrium) P, T phase diagram H_2O

Phase boundary lines in diagrams of unary systems

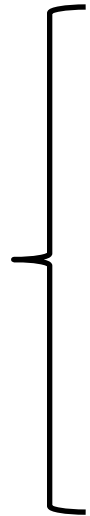
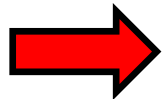
Equilibrium between phases



$$n_g \leftrightarrow n_l$$



$$dn_i \neq 0$$

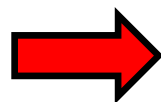


$$dG = VdP - SdT + \sum_i \mu_i dn_i$$

$$\mu_i \equiv \left(\frac{\partial G}{\partial n_i} \right)_{P, T, n_{j \neq i}}$$

The chemical potential of phase i ($i = l, g$) (Study guide p.11-13)

Note: we are dealing with a unary system



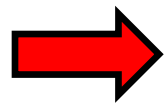
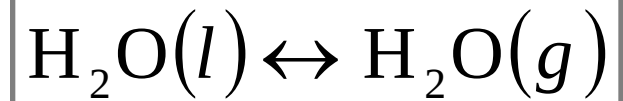
$$\mu_i \equiv G_{i,m}$$

(pure compound)

Phase boundary lines in diagrams of unary systems

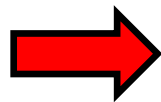
Importance of the chemical potential:

Equilibrium between phases



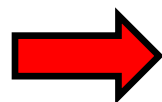
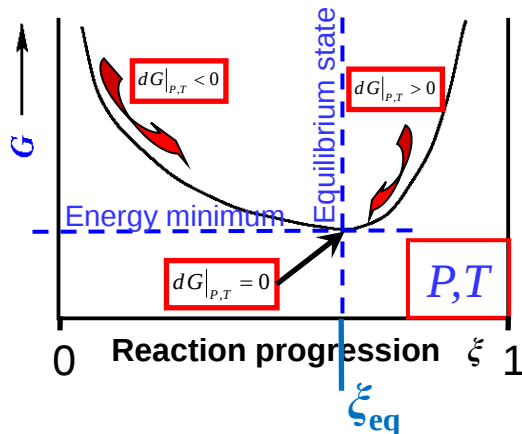
$$dG = VdP - SdT + \mu_l dn_l + \mu_g dn_g$$

Equilibrium



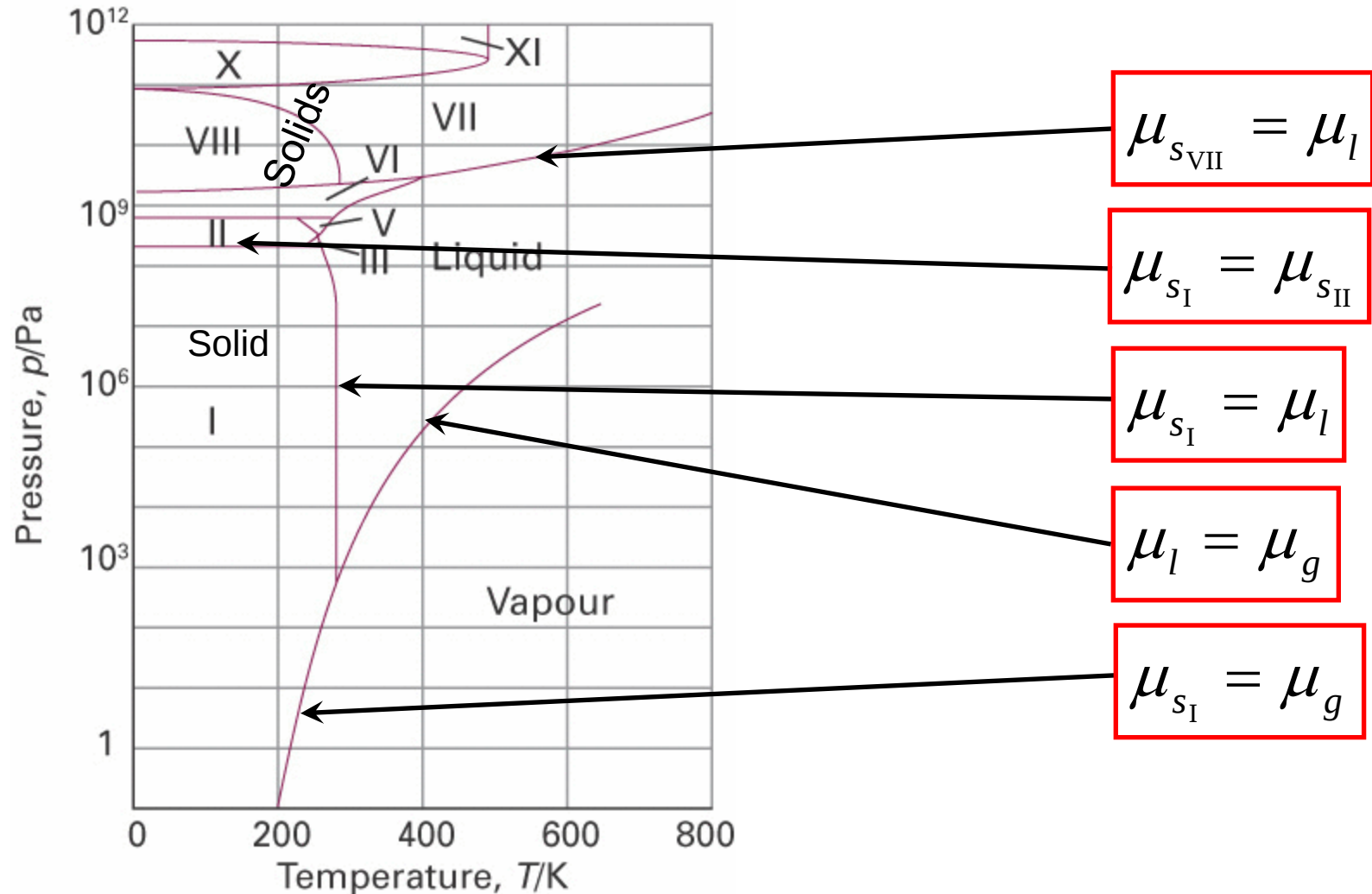
$$dG_{T,P} = 0$$

$$dn_l = -dn_g$$



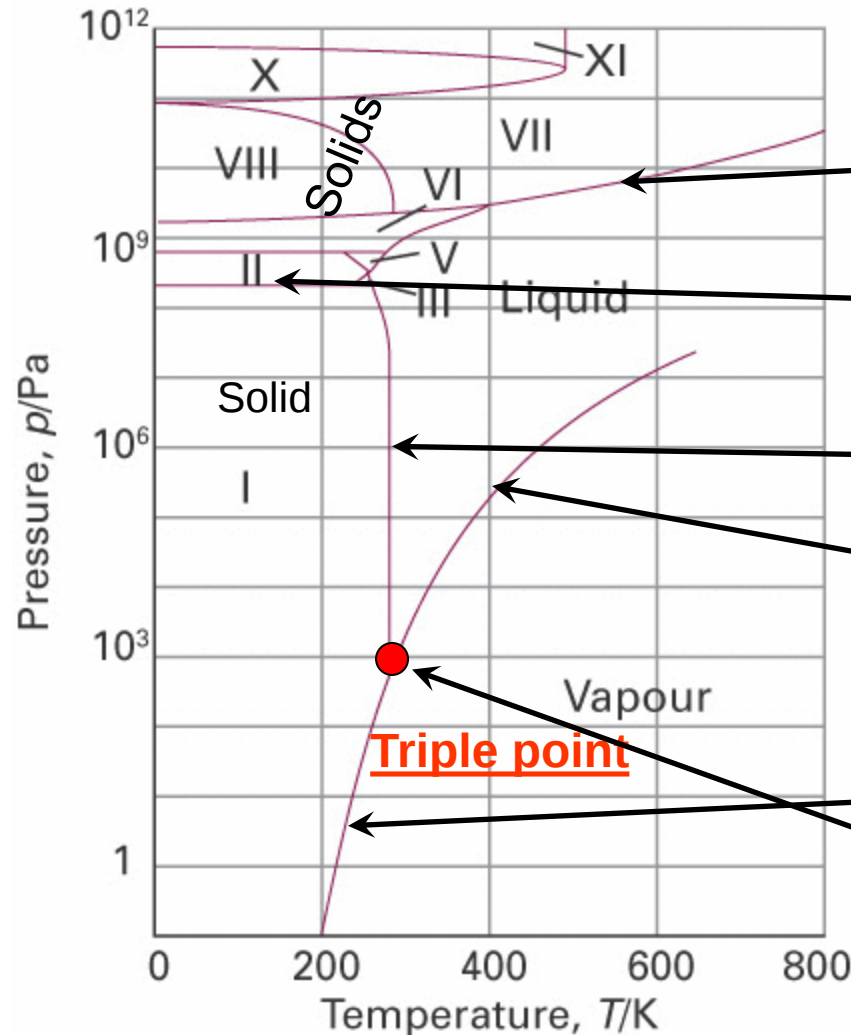
$$\mu_l = \mu_g$$

Phase boundary lines in diagrams of unary systems



(Equilibrium) P, T phase diagram H₂O

Phase boundary lines in diagrams of unary systems



$$\mu_{s_{VII}} = \mu_l$$

$$\mu_{s_I} = \mu_{s_{II}}$$

$$\mu_{s_I} = \mu_l$$

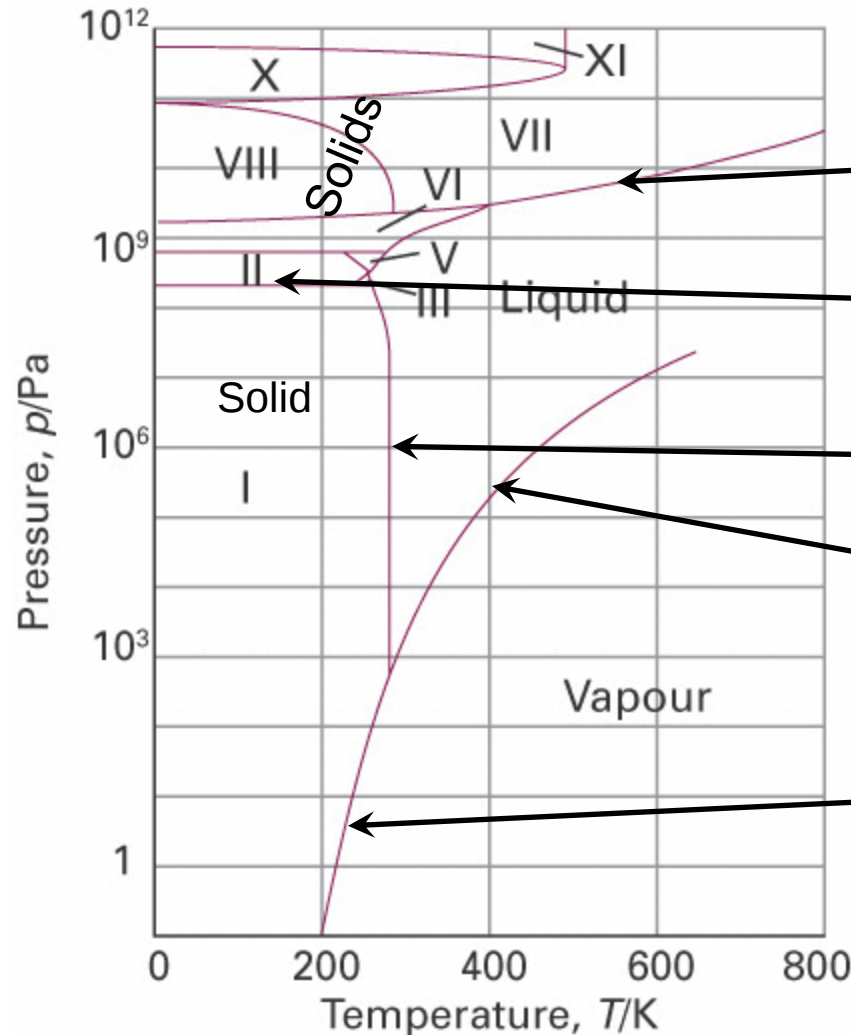
$$\mu_l = \mu_g$$

$$\mu_{s_I} = \mu_g$$

$$\mu_{s_I} = \mu_l = \mu_g$$

(Equilibrium) P, T phase diagram H₂O

Phase boundary lines in diagrams of unary systems



$$G_{s_{VII},m} = G_{l,m}$$

$$G_{s_I,m} = G_{s_{II},m}$$

$$G_{s_I,m} = G_{l,m}$$

$$G_{l,m} = G_{g,m}$$

$$G_{s_I,m} = G_{g,m}$$



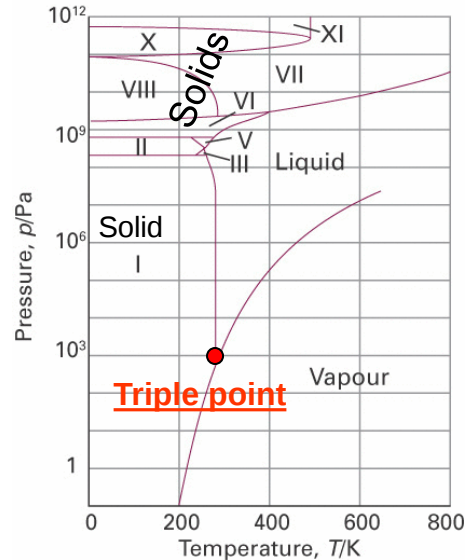
$$\mu_i \equiv G_{i,m}$$

($i = s, l, g$) 28

pure compound:

(Equilibrium) P,T phase diagram H₂O

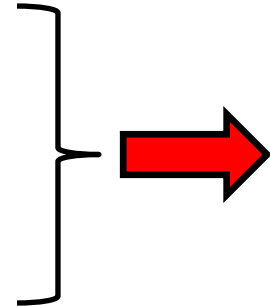
Phase boundary lines in diagrams of unary systems



Along any phase boundary line:
(between two phases α and β)

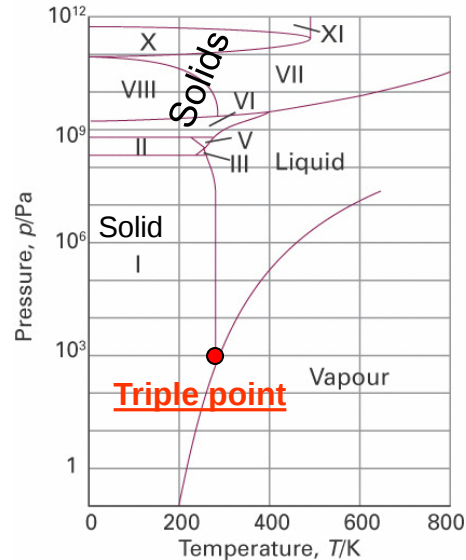
$$dG_{\alpha,m} = dG_{\beta,m}$$

$$dG_{i,m} = V_{i,m} dP - S_{i,m} dT$$



$$V_{\alpha,m} dP - S_{\alpha,m} dT = V_{\beta,m} dP - S_{\beta,m} dT$$

Phase boundary lines in diagrams of unary systems



Along any phase boundary line:
(between two phases α and β)

$$dG_{\alpha,m} = dG_{\beta,m}$$

$$dG_{i,m} = V_{i,m} dP - S_{i,m} dT$$

$$V_{\alpha,m} dP - S_{\alpha,m} dT = V_{\beta,m} dP - S_{\beta,m} dT$$

Clapeyron equation:

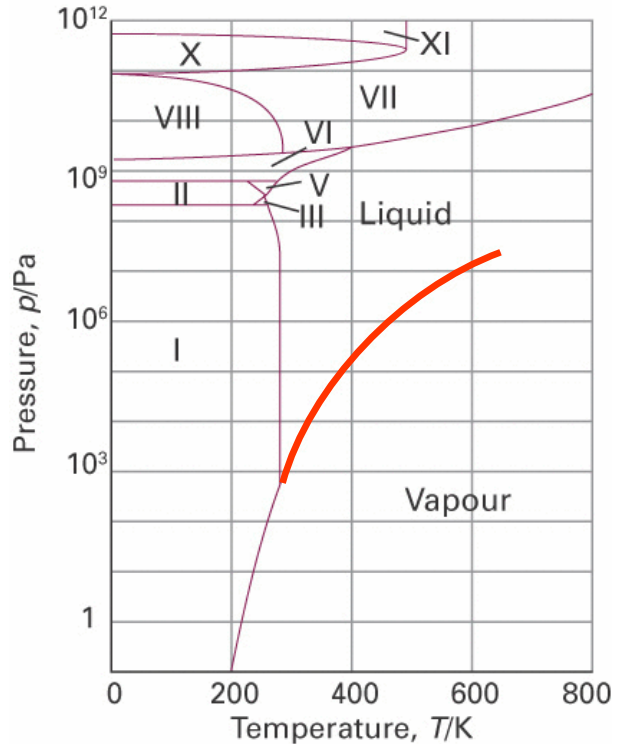
$$\frac{dP}{dT} = \frac{\Delta_{trs} S_m}{\Delta_{trs} V_m}$$

$$\Delta_{trs} G_m = 0$$

$$\frac{dP}{dT} = \frac{\Delta_{trs} H_m}{T_{trs} \Delta_{trs} V_m}$$

(is exact)

Phase boundary lines in diagrams of unary systems



Along *l-g* phase boundary line:

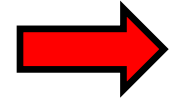
Clapeyron equation:

$$dP = \frac{\Delta_{\text{vap}} H_{\text{m}}}{T_{\text{vap}} \Delta_{\text{vap}} V_{\text{m}}} dT$$

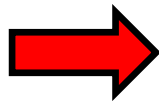
Perfect gas:

$$PV_{\text{m}} = RT$$

$$\Delta_{\text{vap}} V_{\text{m}} \approx V_{\text{g,m}} = \frac{RT}{P}$$

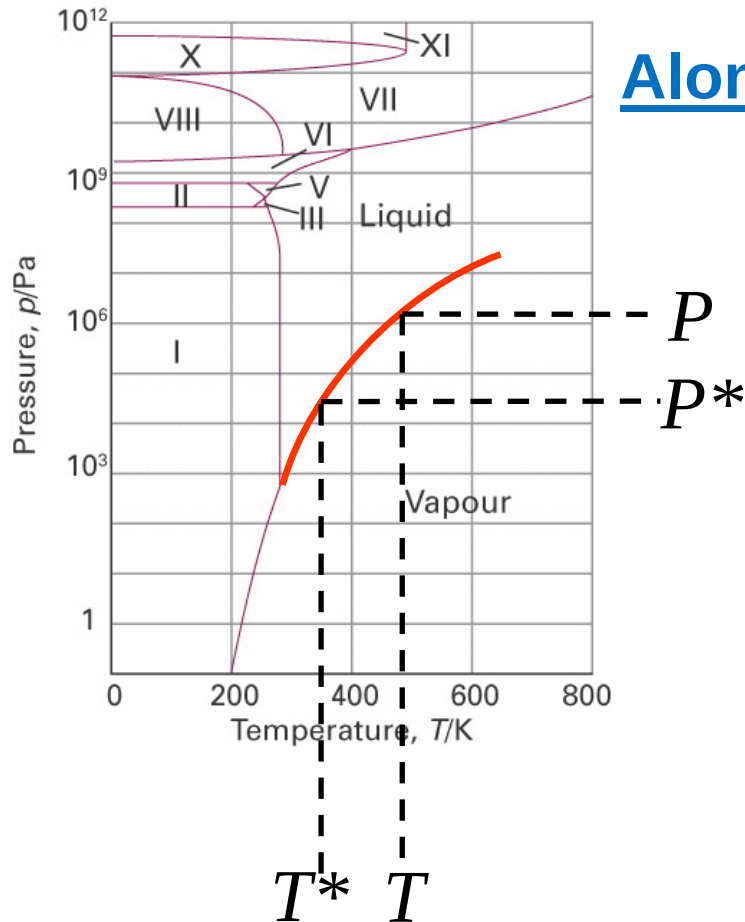


$$\frac{dP}{P} = \frac{\Delta_{\text{vap}} H_{\text{m}}}{RT_{\text{vap}}^2} dT$$



$$\int \frac{dP}{P} = \int \frac{\Delta_{\text{vap}} H_{\text{m}}}{RT_{\text{vap}}^2} dT$$

Phase boundary lines in diagrams of unary systems



Along phase boundary line:

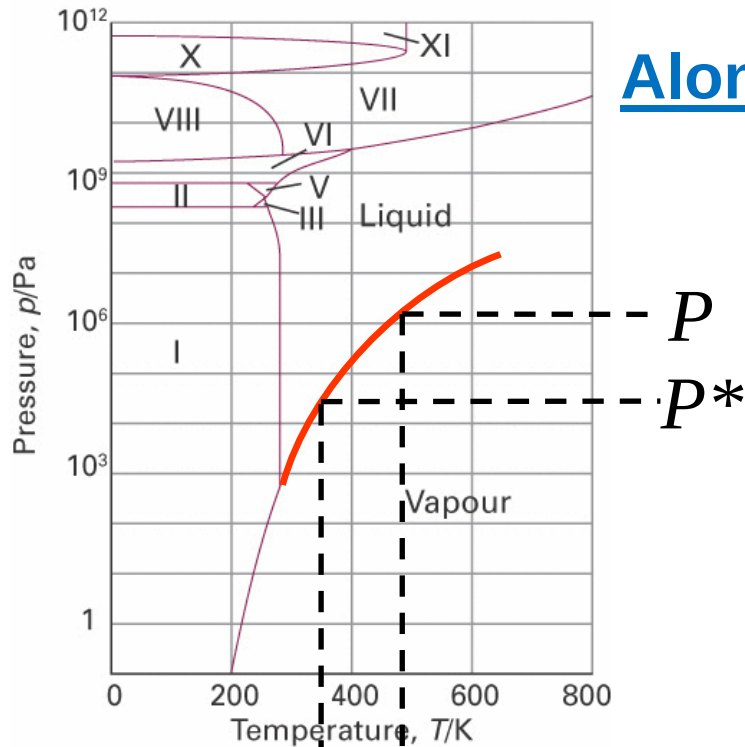
$$\int_{P^*}^P \frac{dP}{P} = \int_{T^*}^T \frac{\Delta_{\text{vap}} H_m}{RT_{\text{vap}}^2} dT$$

$$\Delta_{\text{vap}} H_m(T) \approx \Delta_{\text{vap}} H_m$$

$$\int_{P^*}^P \frac{dP}{P} = \frac{\Delta_{\text{vap}} H_m}{R} \int_{T^*}^T \frac{dT}{T^2}$$

$$\ln \frac{P}{P^*} = - \frac{\Delta_{\text{vap}} H_m}{R} \left[\frac{1}{T} - \frac{1}{T^*} \right]$$

Phase boundary lines in diagrams of unary systems



Along phase boundary line:

Clausius-Clapeyron equation:

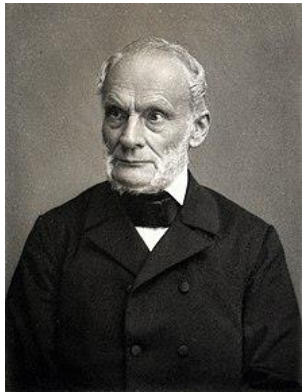
$$\ln \frac{P}{P^*} = - \frac{\Delta_{\text{vap}} H_m}{R} \left[\frac{1}{T} - \frac{1}{T^*} \right]$$



$$P = P^* \exp[-\chi]$$

$$\chi = \frac{\Delta_{\text{vap}} H_m}{R} \left[\frac{1}{T} - \frac{1}{T^*} \right]$$

Clausius-Clapeyron equation



Rudolf Clausius
1822-1888



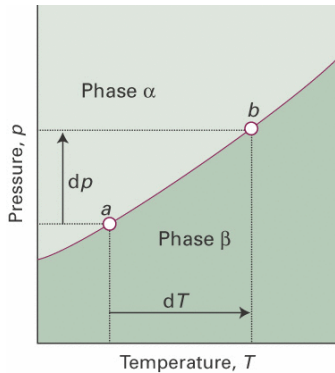
Benoît Clapeyron
1799-1864

Phase boundary lines in phase diagrams of unary systems

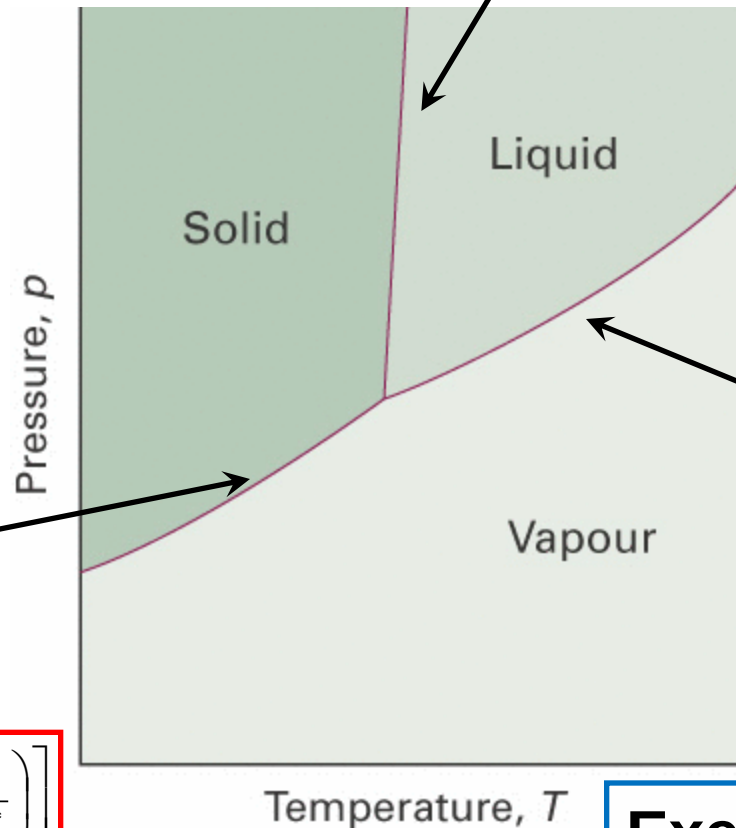
$$\frac{dP}{dT} = \frac{\Delta_{\text{trs}} S}{\Delta_{\text{trs}} V} = \frac{\Delta_{\text{trs}} H}{T_{\text{trs}} \Delta_{\text{trs}} V}$$

Clapeyron

$$\frac{dP}{dT} = \frac{\Delta_{\text{fus}} H}{T_{\text{fus}} \Delta_{\text{fus}} V}$$



$$P \approx P^* + \frac{\Delta_{\text{fus}} H}{\Delta_{\text{fus}} V} \ln \frac{T}{T^*} \approx P^* + \frac{\Delta_{\text{fus}} H}{T^* \Delta_{\text{fus}} V} (T - T^*)$$



$$\frac{dP}{dT} = \frac{\Delta_{\text{vap}} H}{T_{\text{vap}} \Delta_{\text{vap}} V}$$

$$\frac{d \ln P}{dT} \approx \frac{\Delta_{\text{vap}} H}{RT^2}$$

$$P \approx P^* \exp \left[-\frac{\Delta_{\text{vap}} H}{R} \left(\frac{1}{T} - \frac{1}{T^*} \right) \right]$$

Clausius-Clapeyron

$$\frac{dP}{dT} = \frac{\Delta_{\text{sub}} H}{T_{\text{sub}} \Delta_{\text{sub}} V}$$

$$\frac{d \ln P}{dT} \approx \frac{\Delta_{\text{sub}} H}{RT^2}$$

$$P \approx P^* \exp \left[-\frac{\Delta_{\text{sub}} H}{R} \left(\frac{1}{T} - \frac{1}{T^*} \right) \right]$$

Exercise 5-8

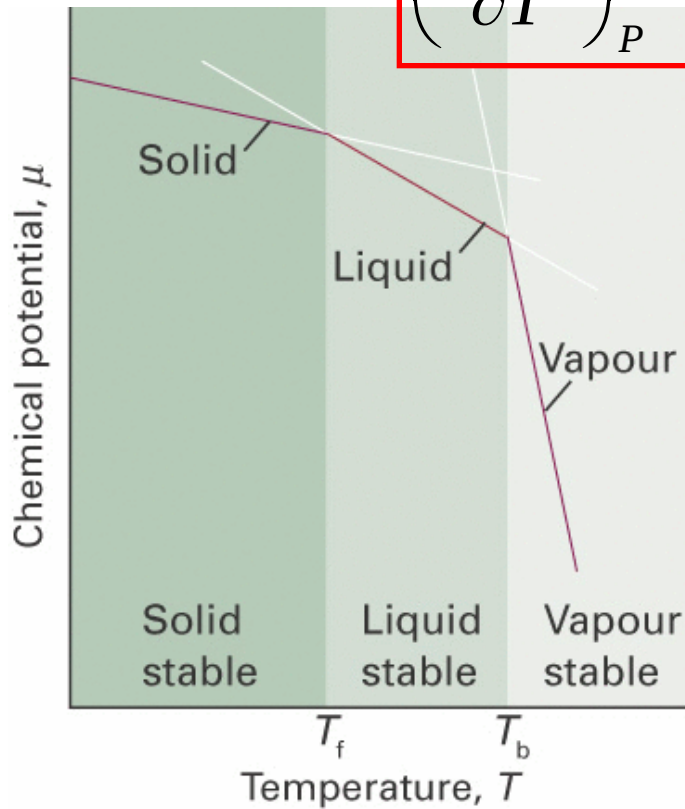
Phase transitions in phase diagrams of unary systems



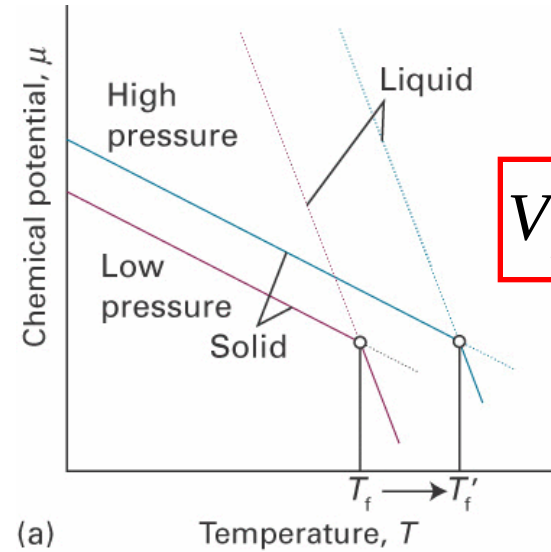
Phase transitions in phase diagrams of unary systems

$$dG_m^\alpha = d\mu^\alpha = V_m^\alpha dP - S_m^\alpha dT$$

$$\left(\frac{\partial \mu^\alpha}{\partial T} \right)_P = -S_m^\alpha$$

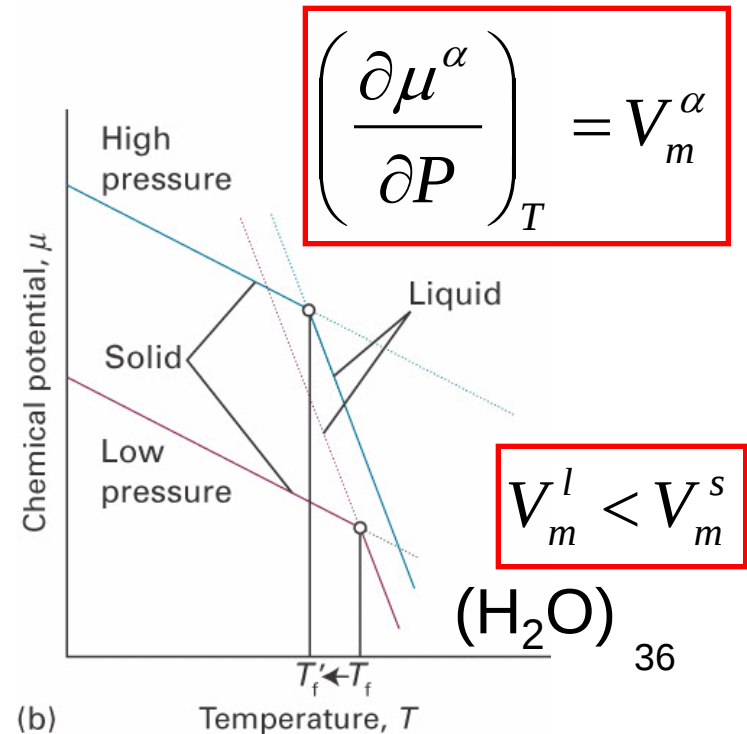


$$S_m^s < S_m^l \ll S_m^g$$



$$V_m^l > V_m^s$$

(a)



$$\left(\frac{\partial \mu^\alpha}{\partial P} \right)_T = V_m^\alpha$$

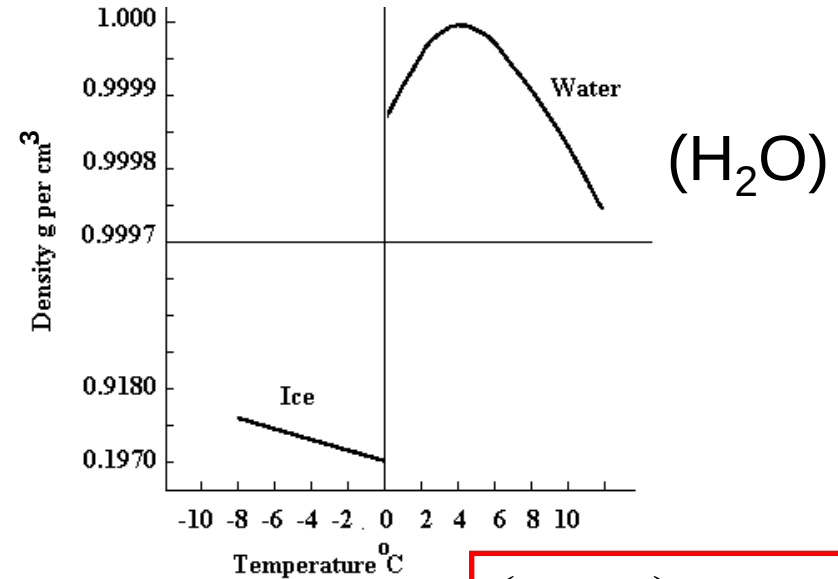
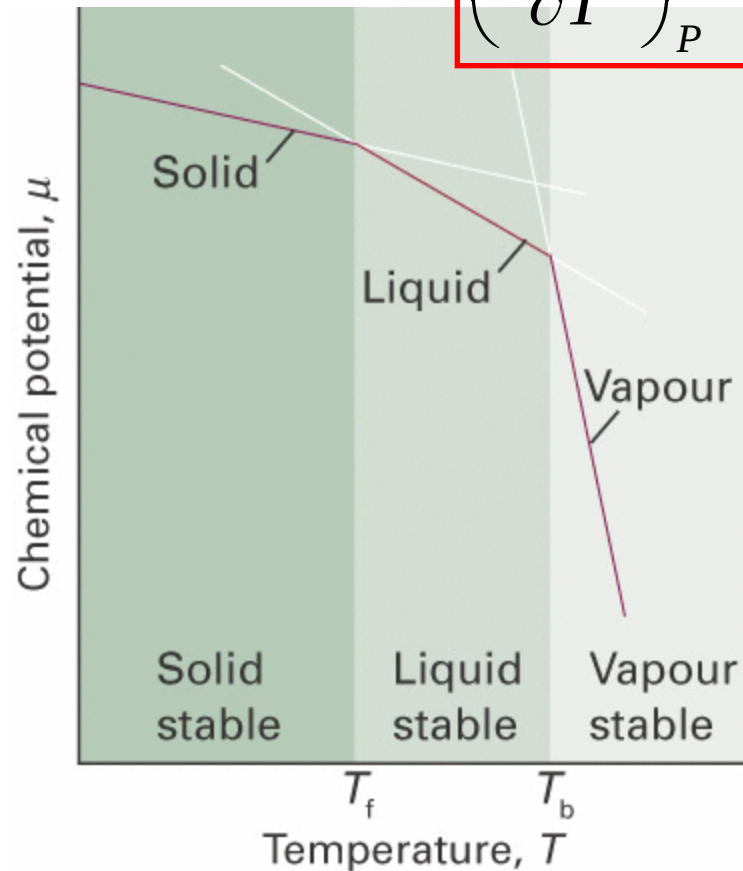
$$V_m^l < V_m^s$$

(H₂O)

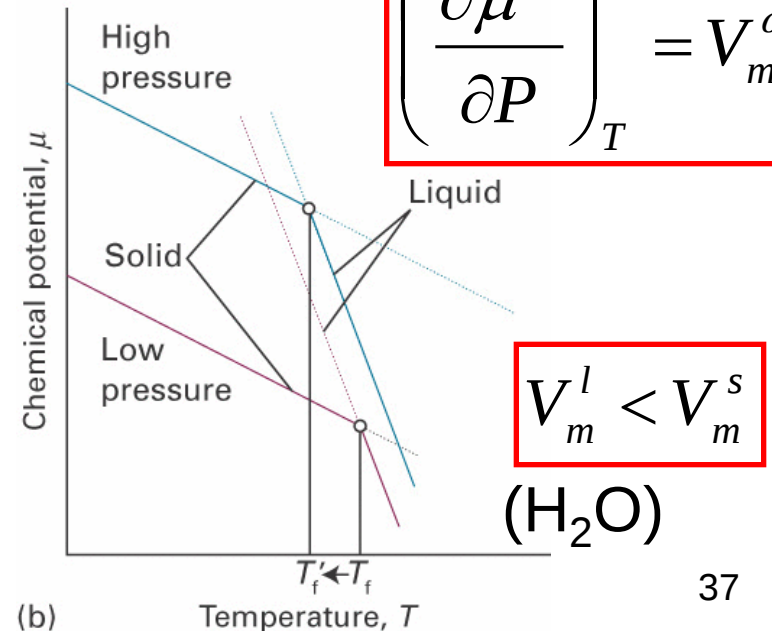
Phase transitions in phase diagrams of unary systems

$$dG_m^\alpha = d\mu^\alpha = V_m^\alpha dP - S_m^\alpha dT$$

$$\left(\frac{\partial \mu^\alpha}{\partial T} \right)_P = -S_m^\alpha$$



$$\left(\frac{\partial \mu^\alpha}{\partial P} \right)_T = V_m^\alpha$$

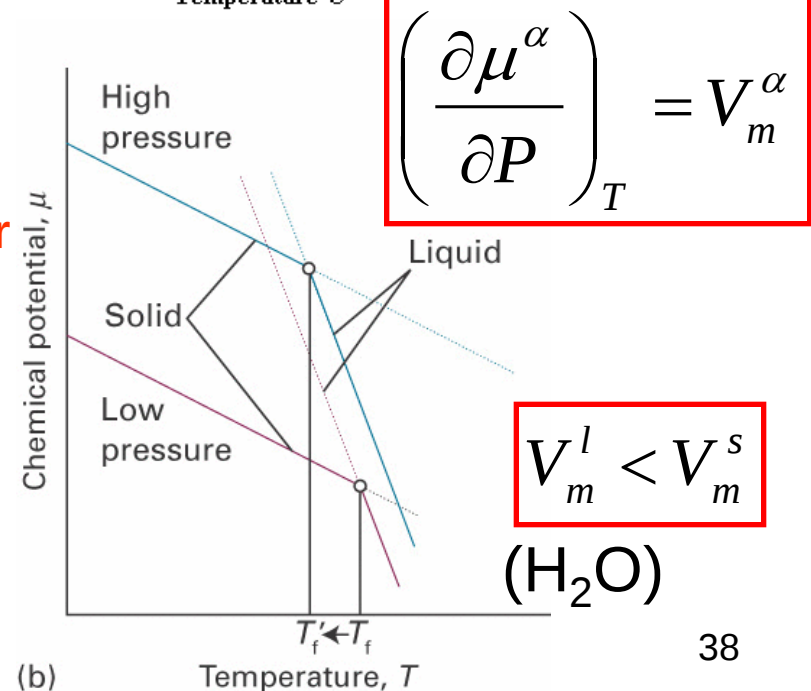
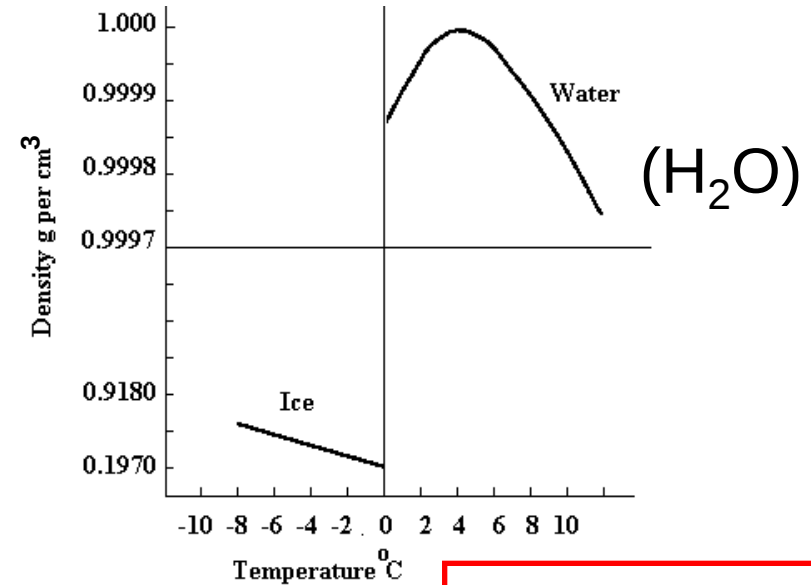
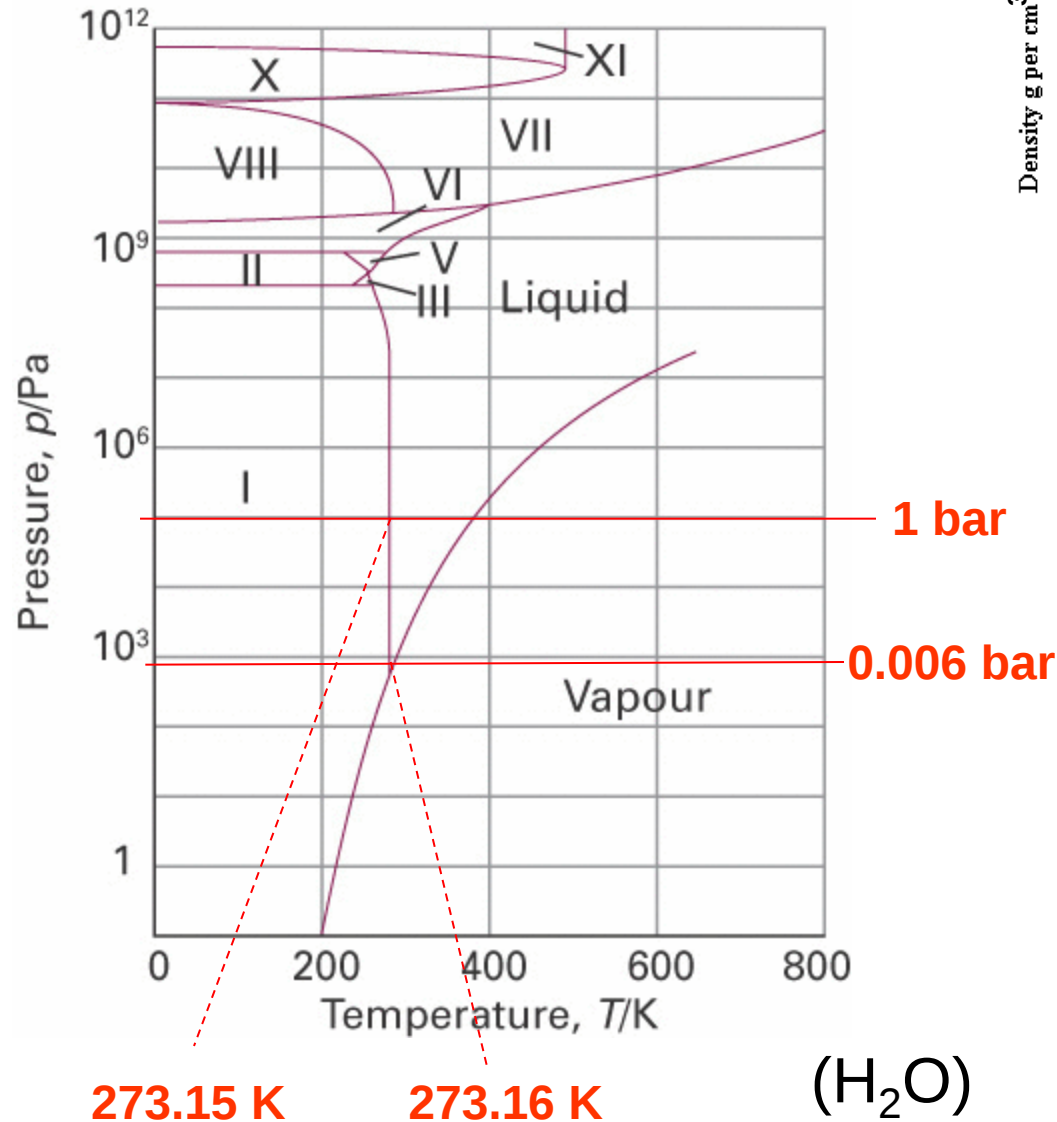


$$V_m^l < V_m^s$$

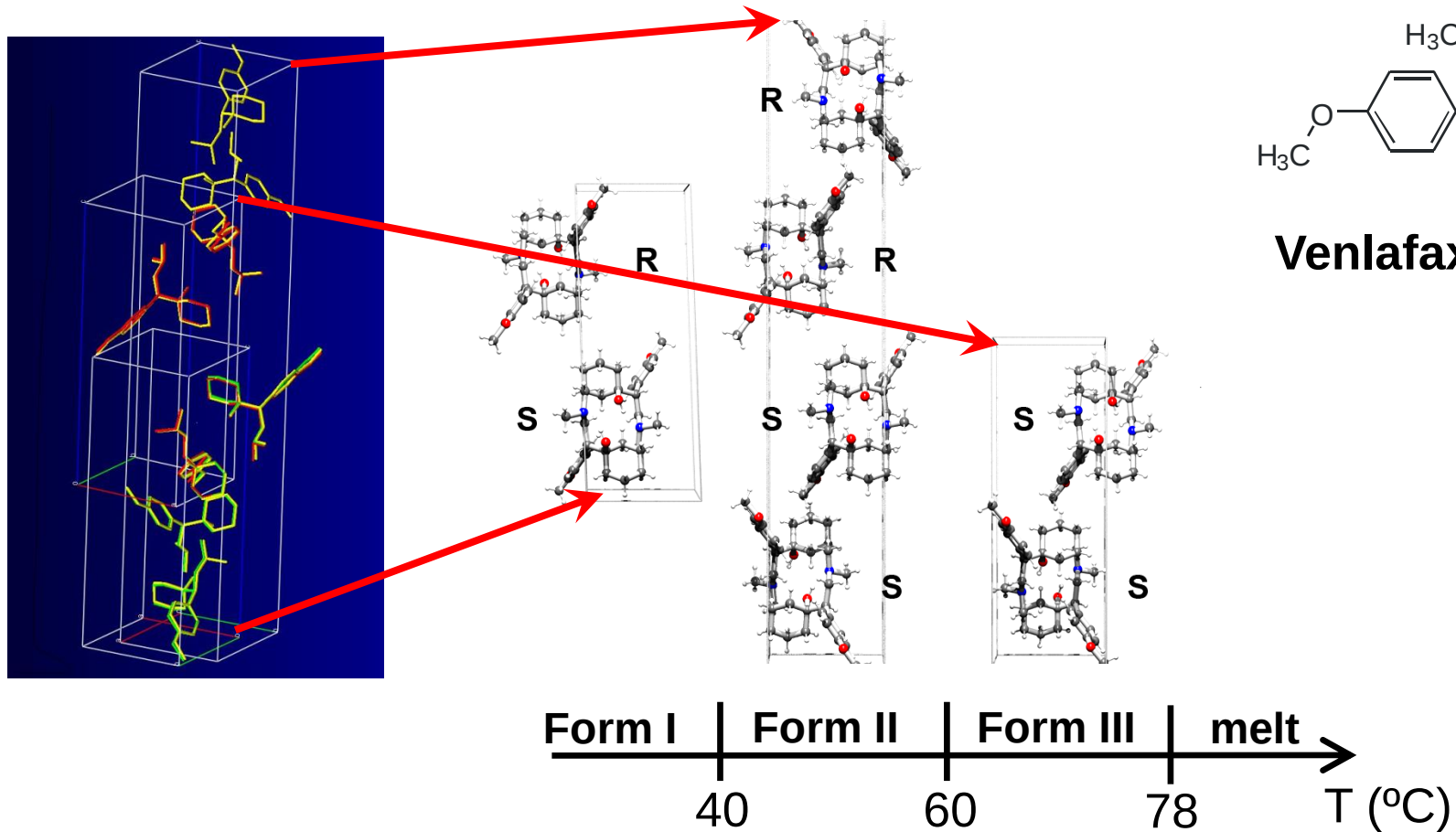
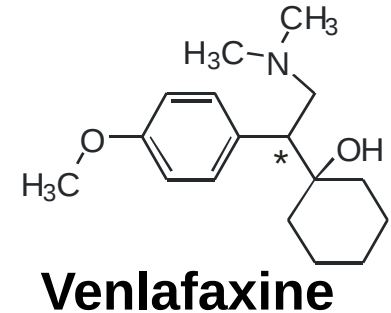
(H₂O)

Phase transitions in phase diagrams of unary systems

$$dG_m^\alpha = d\mu^\alpha = V_m^\alpha dP - S_m^\alpha dT$$

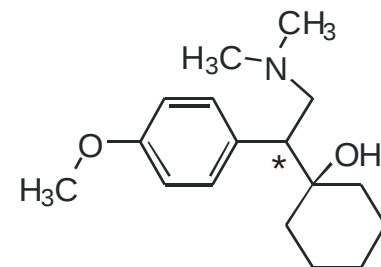
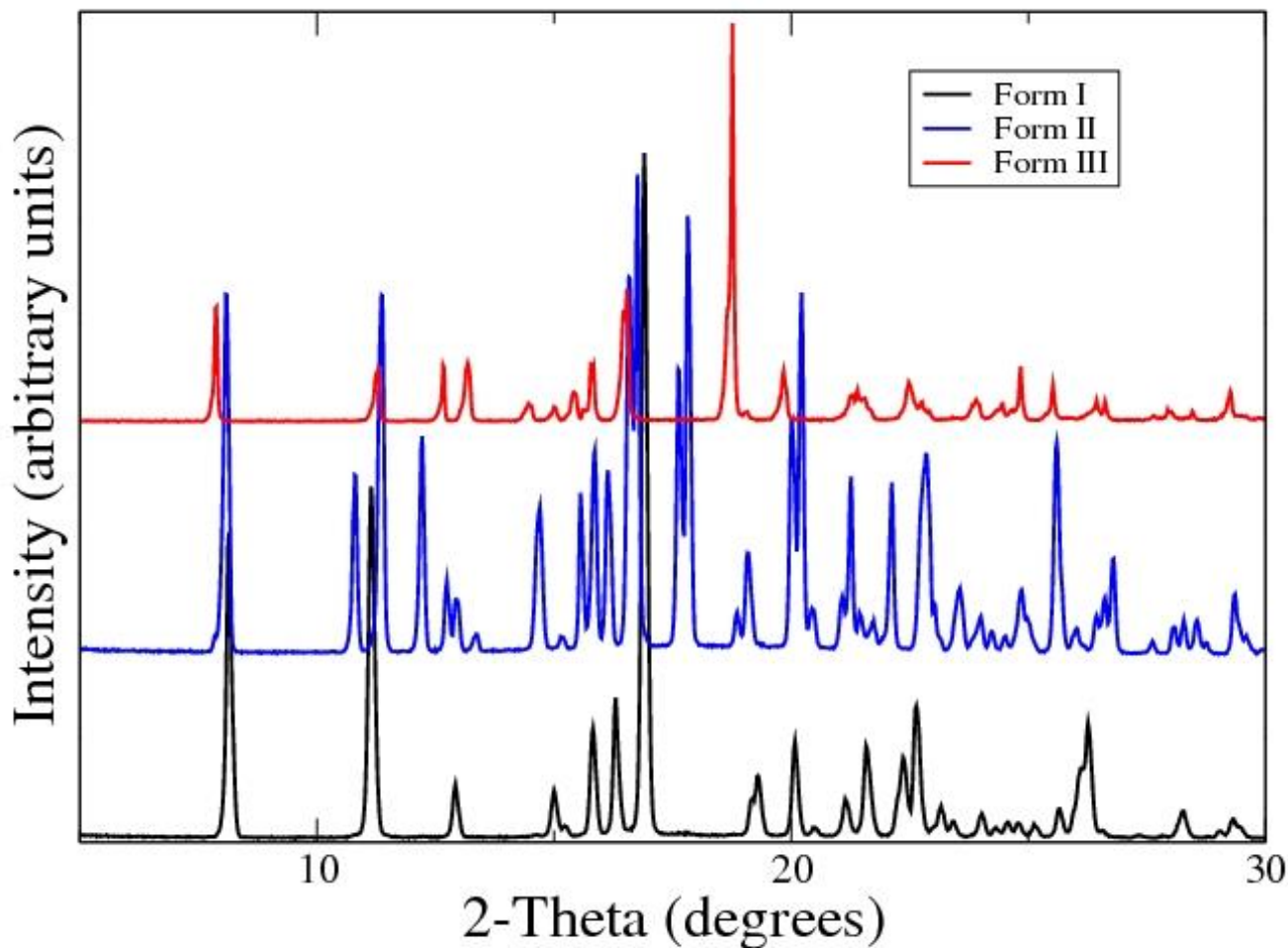


Phase diagrams and phase transitions of unary systems



Polymorphic (solid state) phase transitions

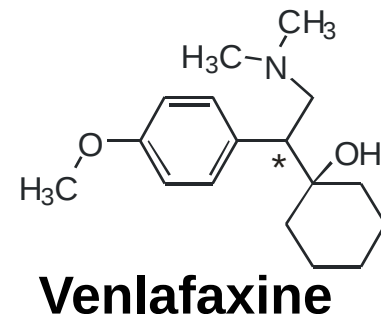
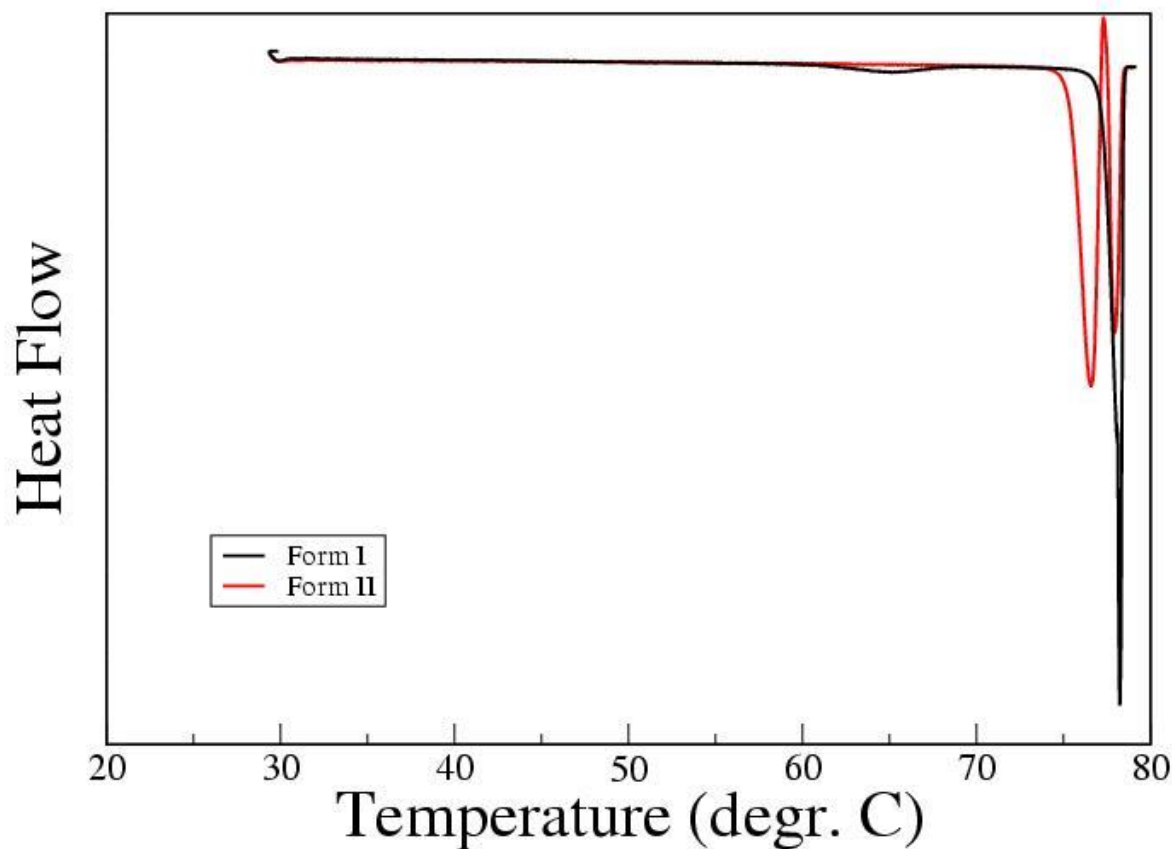
Characterization (polymorphic) crystal structures



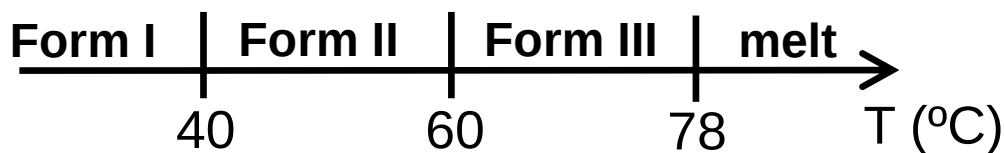
Venlafaxine

Polymorphic forms characterized using
X-Ray (Powder) Diffraction

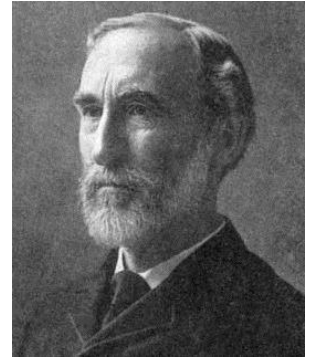
Characterization (polymorphic) phase transitions



Characterized using Differential Scanning Calorimetry

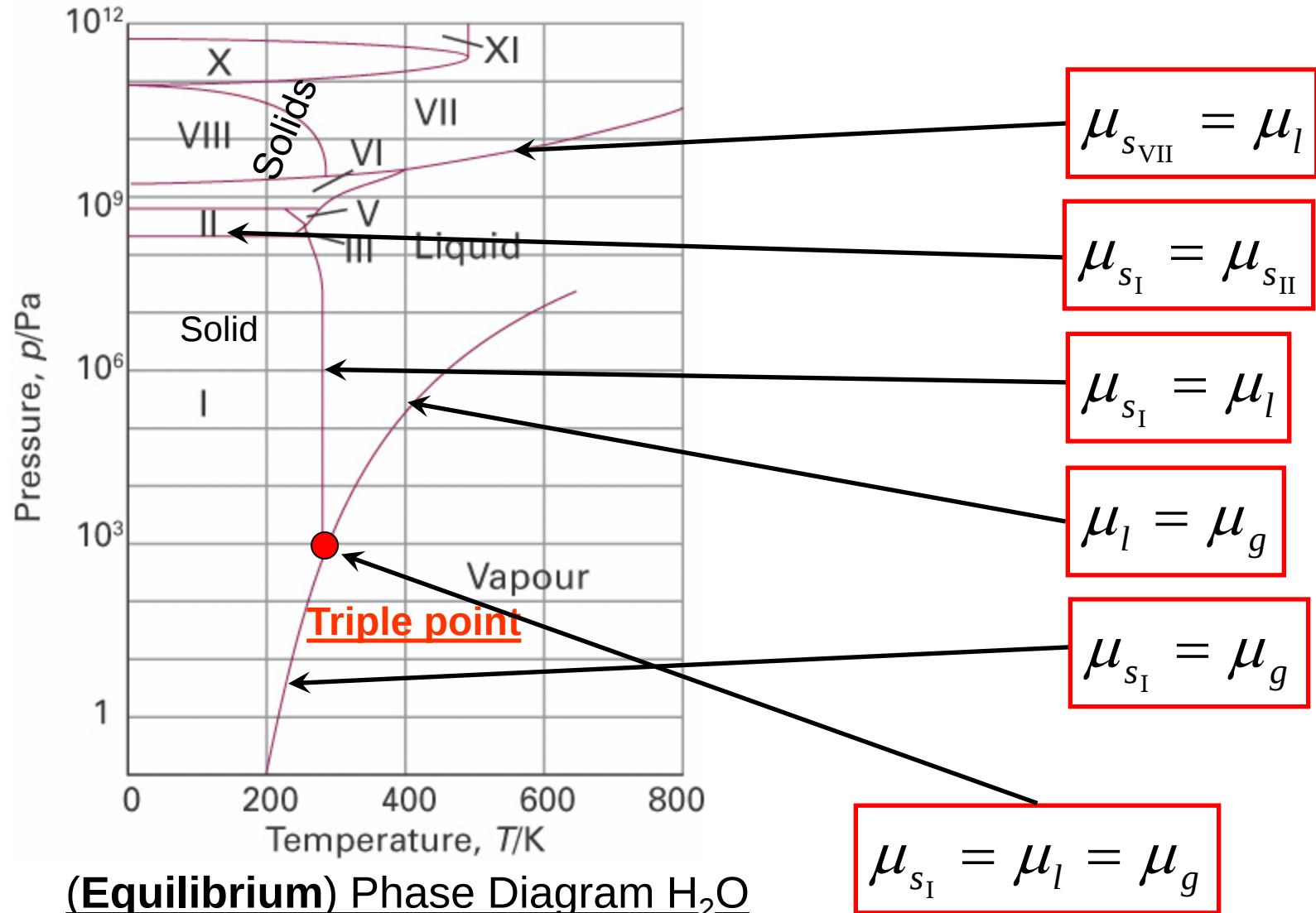


Gibbs phase rule: multicomponent phases



Sneak Preview

Phase boundary lines in diagrams of unary systems



unary phase diagram

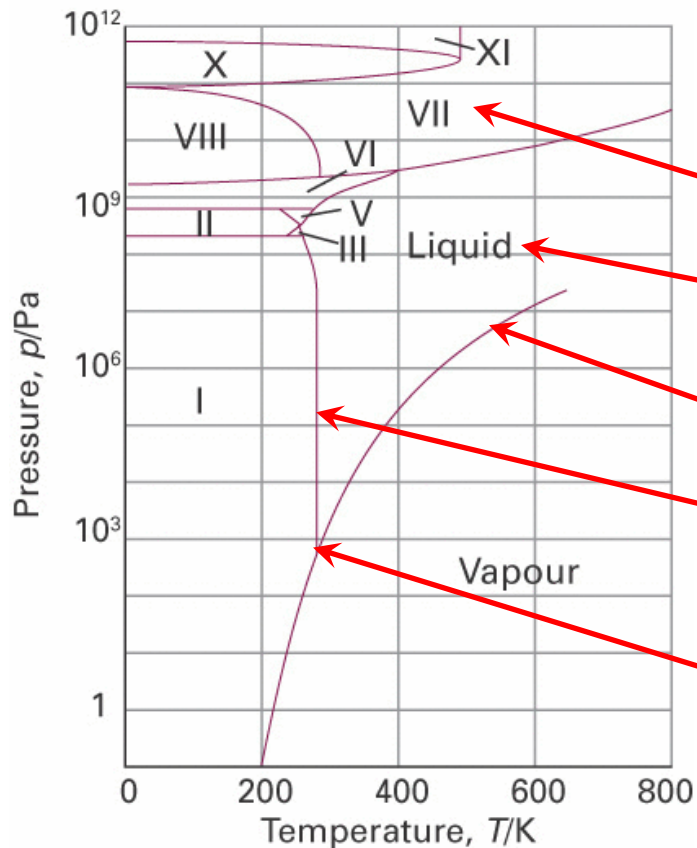
Gibbs phase rule: multicomponent phases

in equilibrium:

$$\mu_{i,\alpha} = \mu_{i,\beta}$$

{ phases $\alpha, \beta, \gamma, \dots$
components $i = 1$

P : # phases in mutual equilibrium



$P = 1$

$P = 2$

$P = 3$

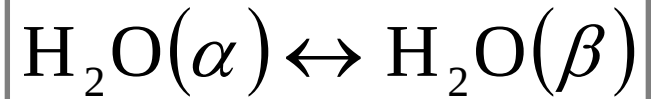
$P = 4?$

What about mixtures of compounds in the phases?

Gibbs phase rule: multicomponent phases

Importance of the chemical potential:

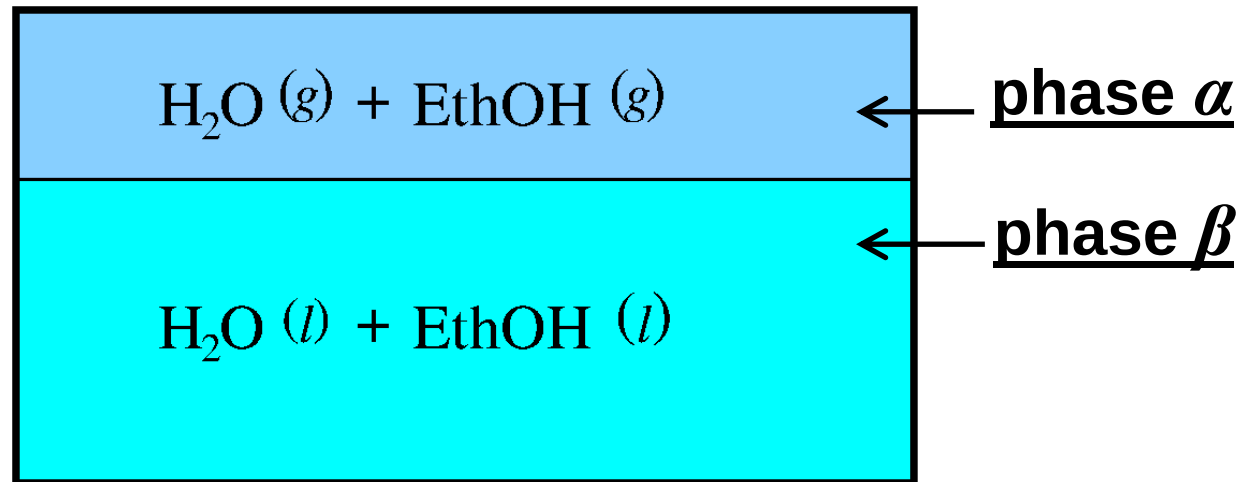
Equilibrium between phases



in equilibrium:

$$\mu_\alpha = \mu_\beta$$

Equilibrium between phases of **components i** in mixtures

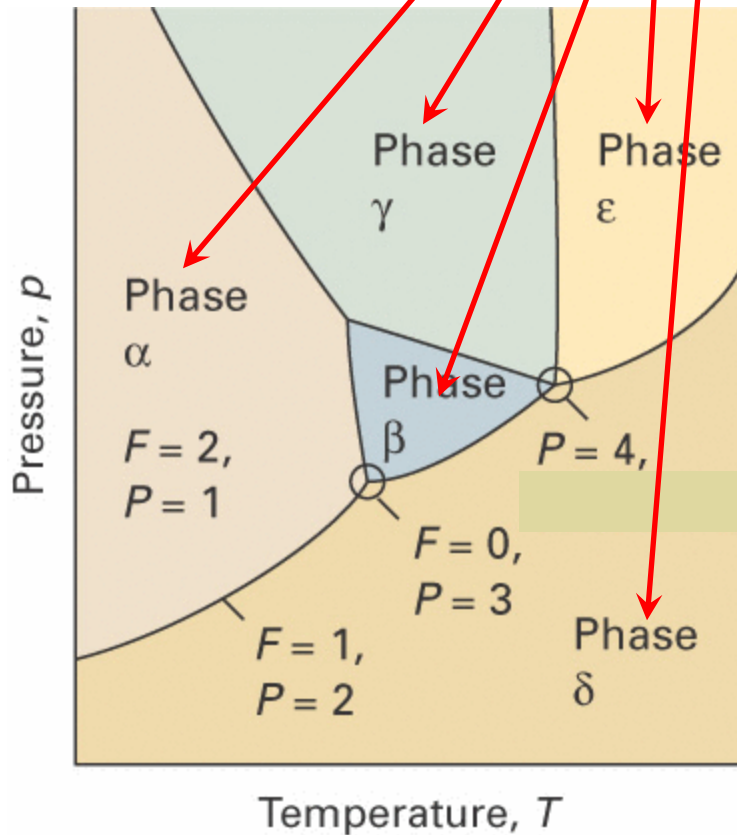
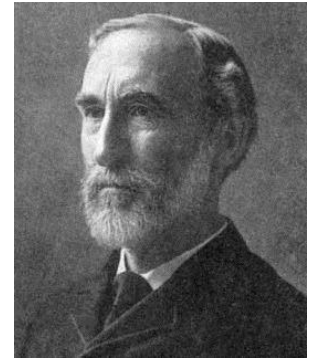


in equilibrium:

$$\mu_{i,\alpha} = \mu_{i,\beta} \left\{ \begin{array}{l} \text{phases } \alpha, \beta \\ \text{components } i \end{array} \right.$$

Gibbs phase rule: unary phase diagrams

$$\left. \begin{array}{l} C = 1 \\ P = 1 \end{array} \right\} \rightarrow F = 2 \quad (T \text{ and } P)$$



Gibbs phase rule

$$F = C - P + 2$$

F : # degrees of freedom

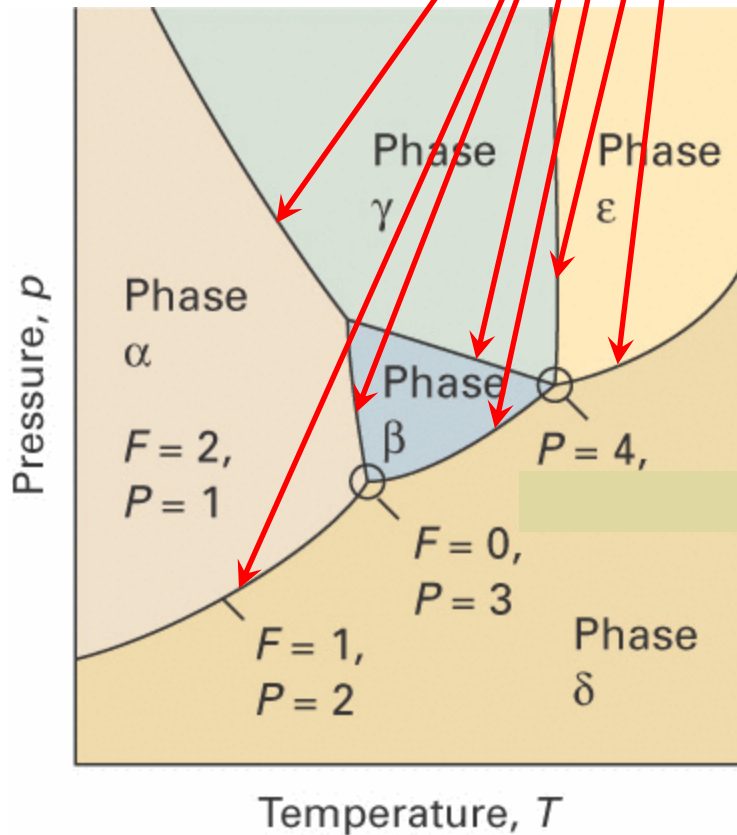
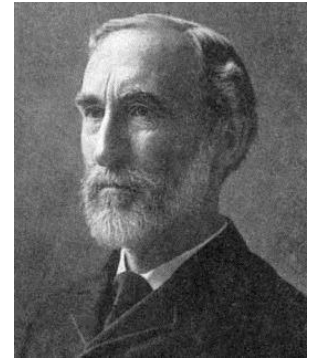
C : # components

P : # phases

unary phase diagram

Gibbs phase rule: unary phase diagrams

$$\left. \begin{array}{l} C = 1 \\ P = 2 \end{array} \right\} \longrightarrow F = 1 \quad (T \rightarrow P \text{ or } P \rightarrow T)$$



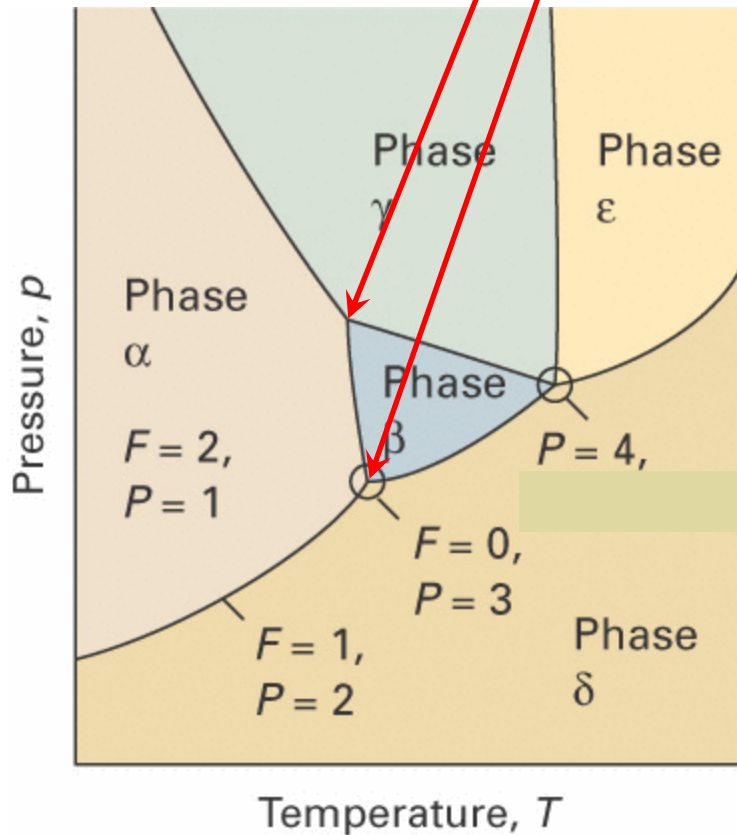
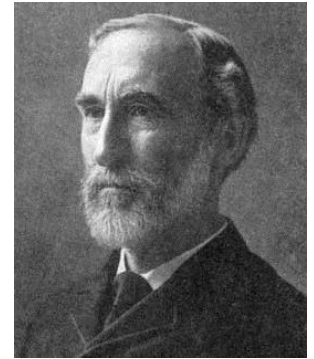
Gibbs phase rule

$$F = C - P + 2$$

unary phase diagram

Gibbs phase rule: unary phase diagrams

$$\left. \begin{array}{l} C = 1 \\ P = 3 \end{array} \right\} \longrightarrow F = 0 \text{ (fixed } T \text{ and } P)$$



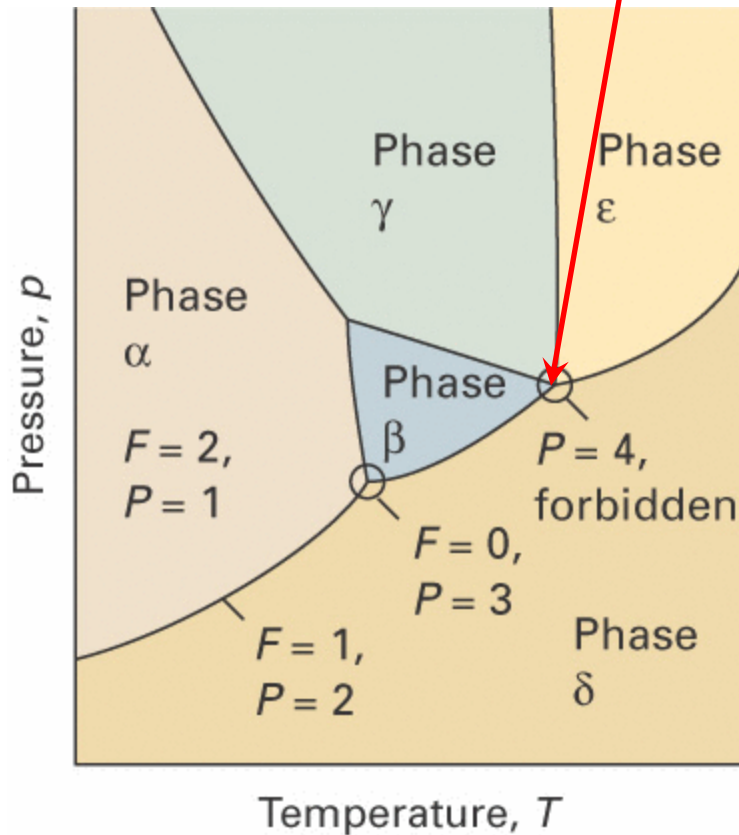
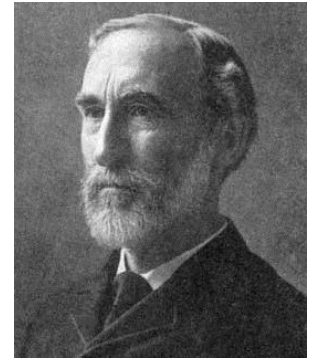
Gibbs phase rule

$$F = C - P + 2$$

unary phase diagram

Gibbs phase rule: unary phase diagrams

$$\left. \begin{array}{l} \cancel{C = 1} \\ \cancel{P = 4} \end{array} \right\} \rightarrow \cancel{F = -1}$$



Gibbs phase rule

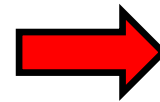
$$F = C - P + 2$$

unary phase diagram

Gibbs phase rule: multicomponent phases

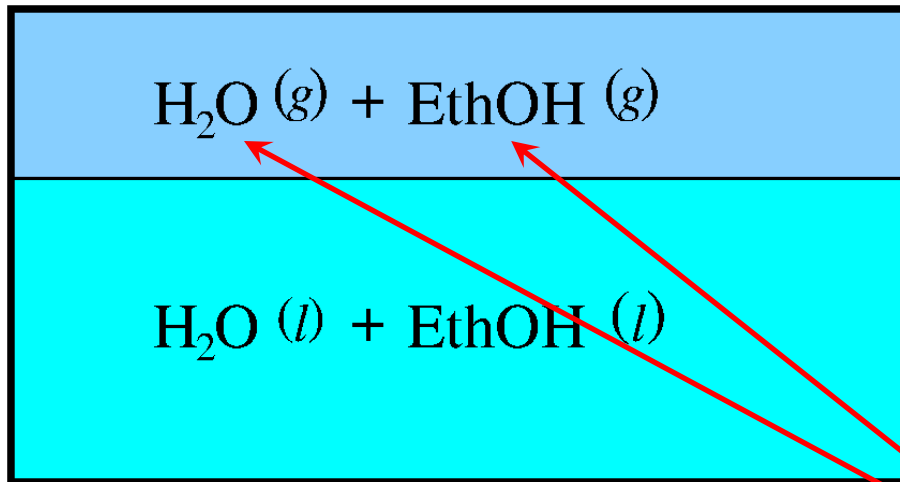
in equilibrium: $\mu_{i,\alpha} = \mu_{i,\beta}$ { phases $\alpha, \beta, \gamma, \dots$
components $i = 1, 2$

C components in each phase



$$x_i \equiv \frac{n_i}{n} = \frac{n_i}{\sum_{j=1}^C n_j}$$

mole fraction of
component i



binary system

$$C = 2$$

So.....?